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Analytical Solutions for a 1D Scale Inhibitor Transport Model with Coupled Adsorption and Precipitation

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Abstract

In a previous publication (Sorbie and Stamatiou in *Transp Porous Media* 123:271–287, 2018), we presented a one-dimensional analytical solution for scale inhibitor transport and retention in a porous medium through a kinetic precipitation mechanism. In this process, a chemical complex of the scale inhibitor precipitates within the porous matrix and it then re-dissolves through a kinetic solubilisation process. Considering the re-dissolution of this precipitate in a one-dimensional linear system such as a reservoir layer or indeed in a laboratory core/pack flood, the flowing aqueous phase gradually dissolves the precipitate which is then eluted from the system. The most novel aspect of this previous analytical solution arose from the fact that, at a certain point in time (or pore volume throughput), the precipitate in the system was locally fully re-dissolved, forming an internal moving boundary between where no precipitate remained (closer to the system inlet) and where a precipitate was present (further into the system up to the outlet). In the current paper, we extend this work by presenting analytical solutions for the case where precipitation/dissolution occurs simultaneously with an adsorption/desorption interaction between the scale inhibitor and the rock surface, described by the nonlinear Langmuir isotherm. When examining this more complex problem in the flow scenario where the local precipitate is completely dissolved, several interesting analytical solution structures are obtained as a result of the internal moving boundary. Which of these structures occurs is rigorously categorised according to the solubility, the initial levels of precipitate and adsorbate, as well as the shape of the Langmuir isotherm. After the mathematical development of the analytical solutions, they are applied to some example problems which are compared with numerical solutions. Finally, a number of different generic features in the scale inhibitor effluent concentration profile are predicted and discussed with regard to practical field applications.

Keywords Scale inhibitors (SIs) · Transport modelling · Flow through porous media · Coupled adsorption and precipitation

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1 Introduction

When water is produced from petroleum reservoirs, it may form certain mineral “scale” deposits, such as calcium carbonate and barium sulphate, because of the aqueous geochemistry of the produced brine, or brine mixtures. In order to prevent the formation of this mineral scale, a production well may be treated with chemical scale inhibitors (SI) in a so-called squeeze treatment. To give a long “squeeze lifetime” in terms of the production of scale inhibitor in the produced brine, the chemical SIs must be retained in the reservoir formation. The main two mechanisms of SI retention within the porous medium are adsorption (denoted Γ) and precipitation (denoted Π) and, in many cases, this also occurs through a coupled adsorption/precipitation (Γ/Π) mechanism.

A major problem for the petroleum industry is the formation and deposition of scale minerals on the downhole equipment and reservoir rock surfaces in contact with formation brine. The most common scaling minerals are calcium carbonate (CaCO_3) and barium sulphate (BaSO_4). Precipitation of these salts occurs when their concentration exceeds their solubility in the formation brine (Stiff and Davis 1952; Miles 1970). These deposits form on the tubing and in the near-wellbore formation and thereby cause a significant reduction of volumetric flow rates, resulting in a decline of oil production (Meyers et al. 1985). One-off chemical treatments to clean the well can restore productivity, but often only for a short period of time. For a more permanent resolution of the problem, the well is treated with scale inhibitors. These chemicals prevent the formation of scale minerals at either the nucleation or crystal growth stages of their deposition (Amjad and Demadis 2015). Scale inhibitor concentrations as small as 5 ppm can be sufficient to accomplish this (King and Warden 1989). For the scale inhibitor (SI) to be effective in reducing scale problems, it must be present in the brine occupying the pore spaces of the rock formation surrounding a producing well. This is achieved in a so-called squeeze treatment (Kerver and Heilhecker 1969; Vetter 1973), in which a volume of high concentration scale inhibitor is injected into the near-well reservoir formation. Production of the well is stopped, and a SI solution is injected. The well is then shut in for a period of time to allow the SI/rock interaction in the pore spaces to reach equilibrium. The SI chemical is retained in the rock formation mainly through two mechanisms: adsorption (denoted Γ ; Trogus et al. 1977; Ramirez et al. 1980; Sorbie et al. 1991, 1992) and precipitation (denoted Π ; Kahrwad et al. 2009; Sorbie 2010, 2012; Vazquez et al. 2010; Zhang et al. 2000). Once production is re-started following the shut-in, the SI chemical then desorbs or dissolves into the formation brine at a concentration which is sufficient to prevent the formation of scale crystals. More recently, there has been some revival of interest in the kinetics of inhibitor adsorption (Khormalia and Moghaddam 2007) and on salt precipitation in porous media (Safari 2014), and this still remains a subject of active research.

The desorption/dissolution of SI into the flowing aqueous phase is a kinetic process, and the treatment could be designed (using modelling) in order to increase the lifetime of a squeeze treatment and hence minimise costs. Mathematical models are invaluable in designing efficient SI squeeze treatments. The rate laws describing the adsorption/desorption and precipitation/dissolution processes must be embedded in a transport equation for flow in porous media. In the present work, we will consider (simplifications of) the following three-dimensional Darcy-scale transport model including kinetic adsorption (Γ) and precipitation (Π):

$$\frac{\partial C}{\partial t} + \mathbf{v} \cdot \nabla C = D \nabla^2 C - \frac{\partial \Pi}{\partial t} - \frac{1 - \phi}{\phi} \frac{\partial \Gamma}{\partial t} \quad (1)$$

$$\frac{\partial \Pi}{\partial t} = \begin{cases} -\kappa(C_s - C), & \text{if } 0 \leq C < C_s, \Pi > 0 \text{ or if } C > C_s \\ 0, & \text{otherwise} \end{cases} \quad (2)$$

$$\frac{\partial \Gamma}{\partial t} = r_a [\Gamma_{\text{eq}}(C) - \Gamma] \quad (3)$$

Here, $\mathbf{x} = (x_1, x_2, x_3) \in \mathbb{R}^3$ is the Cartesian coordinate vector labelling a point in the porous material, $\mathbf{v}(\mathbf{x}, t)$ denotes the (Darcy-scale) fluid velocity field, $C(\mathbf{x}, t)$ is the SI concentration in the mobile phase, $\Pi(\mathbf{x}, t)$ the level of SI precipitate in the pore spaces and $\Gamma(\mathbf{x}, t)$ the amount of SI adsorbed onto the solid surface. The quantities C , Π and Γ are per unit volume of porous material. The dispersion coefficient D and porosity ϕ are assumed to be constants in this model. Precipitation/dissolution rates are given by Eq. (2). This formulation involves a rate constant κ , which can be related to the temperature via the Arrhenius equation (Yuan et al. 1993). The SI solubility C_s in general also depends on field conditions such as temperature and pH (Malandrino et al. 1995), but here we simply assume that there is a critical temperature T_{cp} such that C_s is infinite for $T < T_{\text{cp}}$ and constant for $T \geq T_{\text{cp}}$. Equation (2) further ensures that (1) precipitation can only take place if $C > C_s$ and (2) no dissolution takes place if $\Pi = 0$.

Finally, the adsorption/desorption rate mechanism is described by Eq. (3). Next to a rate constant r_a , it depends largely on a two-parameter Langmuir isotherm, given by

$$\Gamma_{\text{eq}}(C) = \frac{AC}{1 + BC} \quad (4)$$

Both rate Eqs. (2) and (3) appear as source/sink terms in the advection–dispersion equation (2), describing the transport of SI chemical in the bulk fluid. Quite often, with regard to field applications, model equations are written in spherical or cylindrical polar coordinates, which are particularly suitable for describing a near-wellbore geometry (see, for instance, Akanji and Falade 2019). However, in this paper, we will simplify the three-dimensional Cartesian equations (2)–(3) into a one-dimensional form appropriate for the analysis of core-flood experiments (Sect. 2). The reduced set of equations leads to a free-boundary problem which is analytically soluble (Sects. 3–5). A variety of cases are identified. Essential mathematical concepts such as the method of characteristics, weak solutions and shock conditions are utilised, and the reader is referred to Alinhac (2009), Ockendon et al. (2003), Holden and Risebro (2002), Lax (1957) and Smoller (1994) for more details.

2 Mathematical Analysis of Core-Flood Experiments

2.1 Simplified One-Dimensional Model Equations

In a typical core-flood experiment, a *homogeneous* rock core of length L , cross-sectional area A_{core} and porosity ϕ is saturated with a scale inhibitor (SI) solution of concentration $C = C_i$ (stage 1 in Fig. 1). We will assume that the core is oriented in the x_1 -direction. Precipitation occurs when the temperature of the core is raised above T_{cp} and if $C_i > C_s$. At the same time, scale inhibitor adsorption/desorption takes place, and the interaction

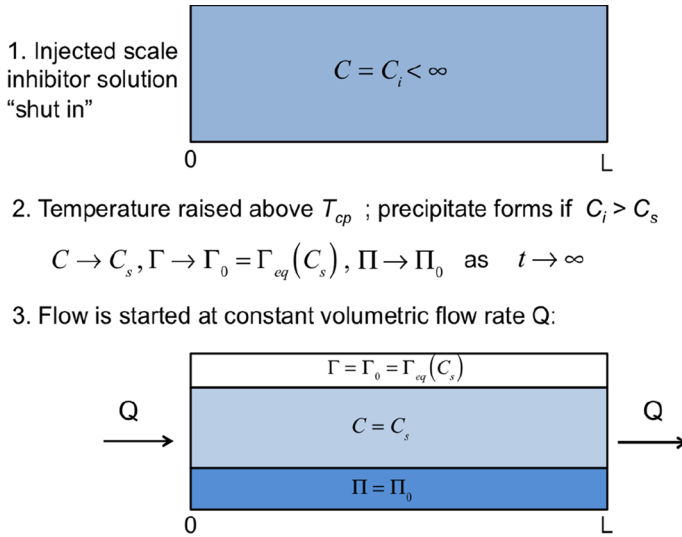


Fig. 1 Illustration of the consecutive stages in a core-flood experiment

of these processes eventually leads to an equilibrium state with uniform levels $C = C_s$, $\Pi = \Pi_0$, $\Gamma = \Gamma_0 = \Gamma_{eq}(C_s)$ throughout the core. After a shut-in (no flow) period during which this equilibrium is reached (stage 2 in Fig. 1), SI-free water ($C = 0$) is injected into the core at constant volumetric flow rate Q (stage 3 in Fig. 1). This translates into a constant linear fluid velocity $v = Q/(A_{core} \cdot \phi)$ (cm s^{-1}) in the x_1 -direction, so that Eqs. (2) and (3) become one-dimensional and we can write $x_1 \equiv x$. Furthermore, we shall assume isothermal conditions, negligible dispersion ($D = 0$) and equilibrium adsorption/desorption ($r_a \rightarrow \infty$). This last condition implies that, for a given mobile phase concentration $C(x, t)$, the adsorption level *instantaneously* becomes $\Gamma_{eq}(C(x, t))$. Then, by the chain rule, $\partial \Gamma / \partial t = \Gamma'_{eq}(C) \partial C / \partial t$ and Eqs. (2)–(3) reduce to

$$\left[1 + \frac{d\Gamma_{eq}}{dC} \right] \frac{\partial C}{\partial t} + v \frac{\partial C}{\partial x} = - \frac{\partial \Pi}{\partial t} \quad (5)$$

$$\frac{\partial \Pi}{\partial t} = \begin{cases} -\kappa(C_s - C), & \text{if } 0 \leq C < C_s, \Pi > 0 \text{ or if } C > C_s \\ 0, & \text{otherwise} \end{cases} \quad (6)$$

where the factor $(1 - \phi)/\phi$ has been accommodated in the Langmuir isotherm coefficient A . The rock core can be represented mathematically as $\Omega := \{(x, t) \in \mathbb{R}^2 : 0 \leq x \leq L, t \geq 0\}$ with U-shaped boundary $\partial \Omega := \{t = 0\} \cup \{x = 0\} \cup \{x = L\}$. In order to solve Eqs. (5)–(6) on the domain Ω , we use the following initial/boundary conditions on $\partial \Omega$:

$$C = C_s, \Pi = \Pi_0, \Gamma = \Gamma_{eq}(C_s) \text{ on } 0 \leq x \leq L \text{ at } t = 0 \quad (7)$$

$$C = 0 \text{ at } x = 0, \text{ for } t > 0 \quad (8)$$

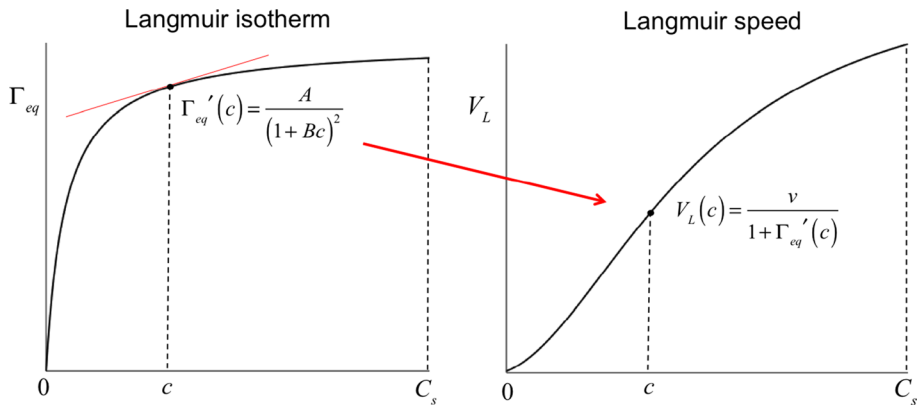


Fig. 2 Construction of the Langmuir speed from the Langmuir isotherm

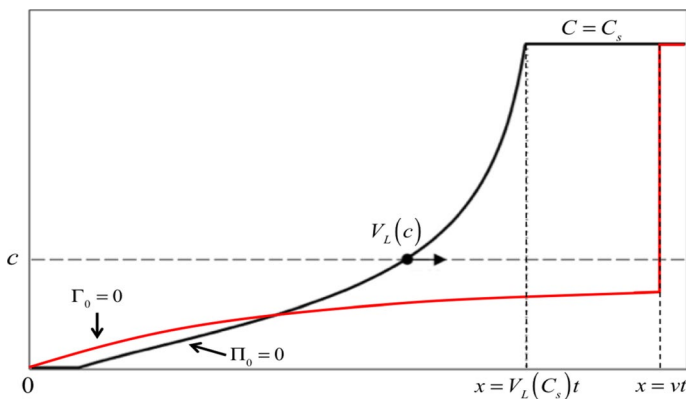


Fig. 3 Rarefaction wave for pure equilibrium desorption ($\Pi_0 = 0$, black curve) compared with the pure dissolution case ($\Gamma_0 = 0$, red curve)

The boundary condition reflects the physical assumption that the concentration at the inlet drops to zero at the start of stage 3 in Fig. 1 ($t = 0$) and remains so for all time.

If there is no precipitate present (i.e. $\Pi_0 = 0$), then $\partial \Pi / \partial t = 0$ and Eq. (5) can be written as $\partial C / \partial t + V_L(C) \partial C / \partial x = 0$, where the term $V_L(C)$ defines the *Langmuir speed* (see Fig. 2) of a concentration value C and is given by

$$V_L(C) := v \left(1 + \frac{d\Gamma_{eq}}{dC} \right)^{-1} = \frac{v(1 + BC)^2}{A + (1 + BC)^2} \quad (9)$$

Since $V_L'(C) > 0$, the PDE $\partial C / \partial t + V_L(C) \partial C / \partial x = 0$ implies that the discontinuity in the data at $x = 0$ develops into a centred rarefaction wave, with each concentration value $c \in [0, C_s]$ travelling at constant velocity $V_L(c)$. This is illustrated in Fig. 3 and contrasted with the “pure dissolution” (i.e. $\Gamma_0 = 0$) solution obtained in a previous paper (Sorbie and Stamatios 2018). Equilibrium desorption causes a retardation of concentration values with respect

to the “water front” moving through the system at velocity v . In the region $V_L(C_s)t \leq x \leq vt$, a bank of $C = C_s$ is sustained. At points behind this bank, the injected water has succeeded in bringing down the concentration level to some $c < C_s$, triggering instantaneous desorption to $\Gamma = \Gamma_{\text{eq}}(c)$, which in turn slows down the transport of the concentration in the x -direction. In contrast to adsorption/desorption, a precipitation/dissolution process aims to restore concentration to full solubility level C_s . We saw that this leads to a discontinuity at the water front, followed by a steady-state region in which dissolution balances the horizontal transport of concentration (see Fig. 3). The question addressed in the current paper is how the two mechanisms combine (i.e. $\Pi_0 \neq 0$, $\Gamma_0 \neq 0$) and interact.

2.2 Solution Method

From Eqs. (5)–(8) we see that $\Pi(0, t) = \Pi_0 - \kappa C_s t$ and therefore the SI precipitate at the inlet is completely dissolved at time t^* , given by

$$t^* = \frac{\Pi_0}{\kappa C_s} \quad (10)$$

Construction of the analytical solution shows that $\Pi(x, t) > 0$ on $[0, L] \times [0, t^*] \setminus \{(0, t^*)\}$. For $t > t^*$, there is a boundary curve, denoted as $x = \alpha_\Pi(t)$, which divides Ω into the subdomains Ω_+ (where $\Pi(x, t) > 0$) and Ω_0 (where $\Pi(x, t) = 0$). This curve will be shown to satisfy a differential equation of the form

$$\frac{d\alpha_\Pi}{dt} = F[C(\alpha_\Pi, t)] \quad (11)$$

Therefore, the boundary curve is entirely determined by the concentration level on it, which itself is “supplied” by the solution in Ω_0 or Ω_+ (see Fig. 4). We will see that if $d\alpha_\Pi/dt > V_L(0)$ at $t = t^*$, there is a time $\tau > t^*$ at which the boundary becomes a straight

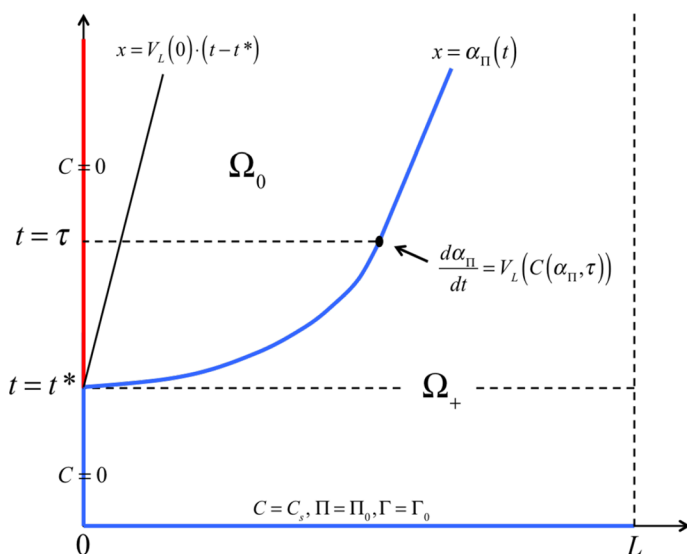


Fig. 4 Schematic of the solution procedure of Eqs. (5)–(8)

line of slope $V_L(C(\alpha_{\Pi}, \tau)) > V_L(0)$. This corresponds to a characteristic projection of Eq. (5) in the domain Ω_0 . For $t^* \leq t < \tau$, the concentration on the boundary curve is given by the solution in Ω_+ , which in turn defines the solution in Ω_0 . For $t \geq \tau$, when the boundary coincides with a characteristic in Ω_0 , the concentration on it remains constant. This will lead to a travelling wave solution region in Ω_+ . Solutions for the various time regions are discussed in turn below for $t < t^*$, while $\Pi > 0$ at the inlet, and for $t > t^*$, when the quantity of precipitate drops to $\Pi = 0$ at the inlet.

3 Solution for $t < t^*$

In this section, we first consider the initial period *before* the precipitate (Π) runs out at the inlet at time t^* .

3.1 Concentration Profile

Equations (5)–(6) with $\Pi > 0$ reduce to a single PDE of the form $a\partial u/\partial x + b\partial u/\partial t = c$ and can be solved analytically by the method of characteristics (see Alinhac 2009; Ockendon et al. 2003 for details). This method constructs the solution u from integral curves of the vector field $(a, b, c) \in \mathbb{R}^3$ defined by the coefficients of the PDE, which themselves may depend on u . In this context, it will be convenient to introduce so-called *characteristic coordinates* $r = r(x, t)$, $s = s(x, t)$. These coordinates are chosen in such a manner that s is a parameter running along the integral curves of the vector field, while r is a parameter describing a space curve Σ_0 which encodes the initial/boundary data accompanying the PDE. The collection of integral curves intersecting Σ_0 then make up the solution surface $u = Z(r, s)$.

For the specific problem of Eqs. (5)–(8), let us imagine that the boundary condition given by Eq. (8) is replaced with an initial condition prescribed on the negative x -axis (outside the domain Ω representing the rock core). We then consider the space curve $\Sigma_0 = \{(r, 0, f(r)) \in \mathbb{R}^3\}$, with the parameter r running along the x -axis and the function $f(r)$ describing arbitrary initial conditions. We can now solve the problem on the entire upper half of the x, t -plane and subsequently choose $f(r)$ to satisfy the initial/boundary conditions in Eqs. (7) and (8).

The *characteristic system* of ordinary differential equations defining the integral curves corresponding to Eq. (5) with $\Pi > 0$ in terms of the parameter s is

$$\frac{dZ}{ds} = \kappa(C_s - Z) \quad (12)$$

$$\frac{dx}{ds} = v \quad (13)$$

$$\frac{dt}{ds} = 1 + \Gamma_{\text{eq}}'(Z) = \frac{A + (1 + BZ)^2}{(1 + BZ)^2} \quad (14)$$

From Eq. (12) and Σ_0 , we obtain the general solution in characteristic coordinates:

$$Z(r, s) = C_s + f(r)e^{-\kappa s} \quad (15)$$

Moreover, Eq. (13) yields $x(r, s) = vs + r$. Introducing the notation $\Gamma_0 := \Gamma_{\text{eq}}(C_s)$ and $\Gamma_0' := \Gamma_{\text{eq}}'(C_s)$, we substitute Eq. (15) into Eq. (14) and integrate to find

$$t(r, s) = \frac{\Gamma_0'}{\kappa} \ln(1 + BZ(r, s)) - \frac{\Gamma_0}{\kappa C_s(1 + BZ(r, s))} + \frac{vs}{V_L(C_s)} + g(r) \quad (16)$$

We now choose the arbitrary function $g(r)$ such that $t(r, 0) = 0$, so

$$g(r) = -\frac{\Gamma_0'}{\kappa} \ln(1 + BZ(r, 0)) + \frac{\Gamma_0}{\kappa C_s(1 + BZ(r, 0))} \quad (17)$$

From Eq. (14), we see that $\partial t / \partial s > 0$ and hence

$$t = 0 \Leftrightarrow s = 0 \Leftrightarrow x = r \quad \text{and} \quad t > 0 \Leftrightarrow s > 0 \Leftrightarrow x > r \quad (18)$$

We now express the initial/boundary conditions given by Eqs. (7) and (8) in the r, s -coordinates in order to determine the function $f(r)$. Using Eq. (18), we find that the initial condition $C(x, 0) = C_s$, $0 \leq x \leq L$ is equivalent to $Z(r, 0) = C_s + f(r) = C_s$, $0 \leq r \leq L$. Moreover, since $x = 0$ if and only if $r = -vs$, it follows that the boundary condition $C(0, t) = 0$, $t > 0$ is equivalent to $Z(r, -r/v) = C_s + f(r) \exp(\kappa r/v)$, $r < 0$. Thus, the required function is

$$f(r) = \begin{cases} 0, & r \geq 0 \\ -C_s e^{-\kappa r/v}, & r < 0 \end{cases} \quad (19)$$

In order to single out a point on the discontinuity at $r = 0$ we introduce an auxiliary parameter $\lambda \in [0, 1]$ and let $f(0) = (\lambda - 1)C_s$. This will allow us to distinguish between the characteristic projections emanating from the origin.

At $t = 0$, we have $r = x$ and therefore $Z(r, 0) = C(x, 0) = C_s + f(x)$. This is shown in Fig. 5. The feed condition $C(0, t) = 0$, $t > 0$ is accommodated by an initial condition $C(x, 0) = C_s - C_s e^{-\kappa x/v}$ on $-\infty < x < 0$. We will proceed to consider what is happening on the larger domain $(-\infty, L] \times [0, \infty)$ and subsequently restrict attention to Ω .

Using $x = vs + r$ we can eliminate s from Eqs. (15) and (16) by defining $\tilde{C}(x, r)$ and $\tilde{t}(x, r)$ as follows:

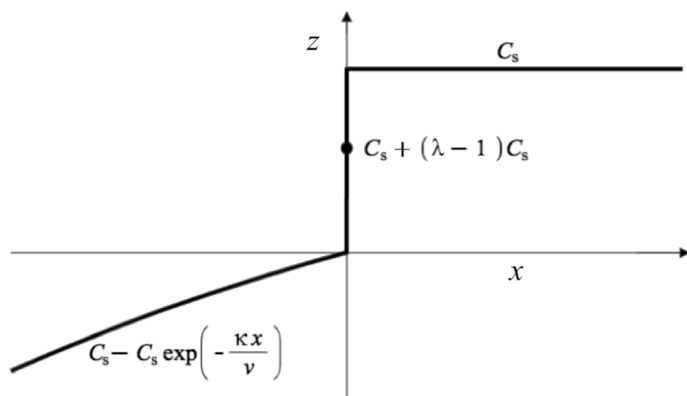


Fig. 5 Initial conditions for Eq. (5) on $-\infty \leq x \leq L$ are chosen to satisfy $C(x, 0) = C_s$ on $[0, L]$ and $C(0, t) = 0$ for $t > 0$

Fig. 6 Characteristic projections of Eq. (5) with initial conditions given by Eq. (19), which are shown in Fig. 5

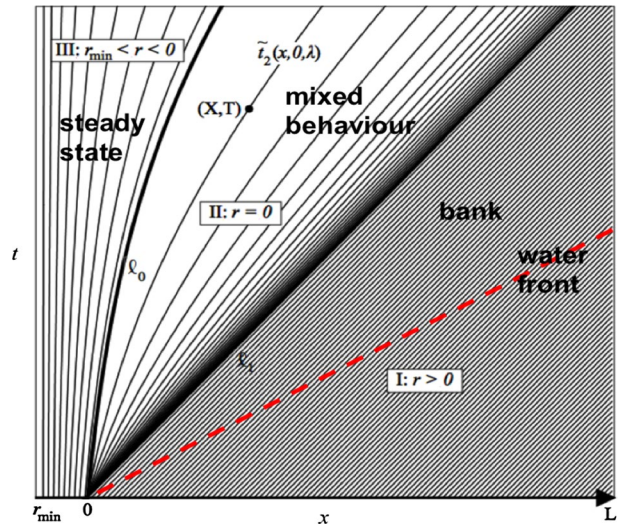
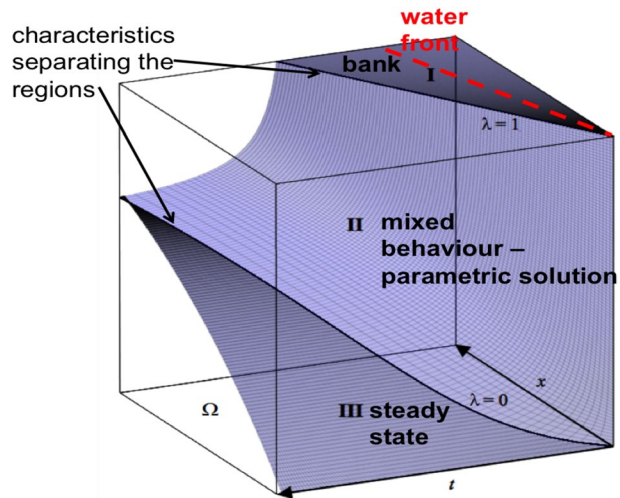


Fig. 7 Solution surface consisting of the characteristics of Eq. (5)



$$\tilde{C}(x, r) := Z\left(r, \frac{x-r}{v}\right) = C_s + f(r)e^{k(r-x)/v}, \quad \tilde{t}(x, r) := t\left(r, \frac{x-r}{v}\right) \quad (20)$$

We note that $\tilde{t}(x, r) \in [0, \infty)$ if and only if $x \geq r > r_{\min}$, where

$$r_{\min} := -\frac{v}{k} \ln\left(\frac{1 + BC_s}{BC_s}\right) \quad (21)$$

According to the different components of the piecewise function $f(r)$, we distinguish solutions regions I, II and III (see Figs. 6, 7). The solutions in these regions will be denoted by $\tilde{C}_1, \tilde{C}_2, \tilde{C}_3$ in the x, r coordinates and by C_1, C_2, C_3 in the x, t coordinates.

Region I $r > 0$ and hence $\tilde{C}_1(x, r) = C_s$. The characteristics $t = \tilde{t}_1(x, r) = (x - r)/V_L(C_s)$ are straight lines. We can invert to find $r = x - V_L(C_s)t$ and therefore the explicit solution $C_1(x, t) = C_s$. There is a widening bank of constant concentration $C = C_s$ behind the advancing water front. This is purely due to equilibrium desorption.

Region II: here, $r = 0$ and hence $\tilde{C}_2(x, 0) = C_s + f(0)e^{-\kappa x/v}$. The auxiliary parameter $\lambda \in [0, 1]$ is now used to pick a value of $f(0)$, and we may write the solution as

$$\tilde{C}_2(x, \lambda) = C_s + (\lambda - 1)C_s e^{-\kappa x/v} \quad (22)$$

and

$$\begin{aligned} \tilde{t}_2(x, \lambda) = & \frac{x}{V_L(C_s)} + \frac{\Gamma_0'}{\kappa} \ln \left(\frac{1 + B\tilde{C}_2(x, \lambda)}{1 + \lambda BC_s} \right) \\ & + \frac{\Gamma_0}{\kappa C_s} \left[\frac{1}{1 + \lambda BC_s} - \frac{1}{1 + B\tilde{C}_2(x, \lambda)} \right] \end{aligned} \quad (23)$$

The characteristics are the curves $t = \tilde{t}_2(x, \lambda)$, with the curve $\ell_0 := \{t = \tilde{t}_2(x, 0)\}$ and the line $\ell_1 := \{t = \tilde{t}_2(x, 1)\}$ bounding region II. It will sometimes be convenient to write $\tilde{t}_2(x, 0, \lambda)$ and $\tilde{C}_2(x, 0, \lambda)$ to emphasise the correspondence with $r = 0$.

Given a point (X, T) in region II such as illustrated in Fig. 6, we can use Eq. (23) to find the unique value of λ such that $\tilde{t}_2(X, \lambda) = T$. The concentration level $\tilde{C}_2(X, \lambda)$ at (X, T) is then found using Eq. (22). This parametric description is the closest we can get to an explicit solution of Eq. (5) in region II. As stated in Fig. 6, dissolution and desorption occur simultaneously in this zone of mixed behaviour.

Region III: here, $r_{\min} < r < 0$, and hence $\tilde{C}_3(x, r) = C_s - C_s e^{-\kappa x/v}$. Thus, for a fixed value of x , the concentration remains constant, while $\tilde{t}(x, r)$ varies with r . In other words, the concentration in this region is independent of t and we can write

$$C_3(x) = C_s - C_s e^{-\kappa x/v} \quad (24)$$

We recognise this as the steady-state solution of Eq. (5). Since $\partial C_3/\partial t = 0$, no (equilibrium) desorption occurs in this region. The characteristic projections are the curves

$$\begin{aligned} t = \tilde{t}_3(x, r) = & \frac{x}{V_L(C_s)} + \frac{\Gamma_0'}{\kappa} \ln \left(\frac{1 + BC_3(x)}{1 + BC_3(r)} \right) \\ & + \frac{\Gamma_0}{\kappa C_s} \left[\frac{1}{1 + BC_3(r)} - \frac{1}{1 + BC_3(x)} \right] \end{aligned} \quad (25)$$

This establishes the analytical solution for the mobile phase chemical concentration, $C(x, t)$, for $t < t^*$, as comprised of three components.

3.2 Precipitate Profile

We now use the concentration profile, $C(x, t)$, derived above to construct an expression for Π on Ω . If $\Pi > 0$, Eq. (6) yields

$$\Pi(x, t) = \kappa \int [C(x, t) - C_s] dt \quad (26)$$

This integral is straightforward to compute in regions I and III. With $C_1(x, t) = C_s$ it follows that $\Pi_1(x, t) = \Pi_0$, since the initial condition $\Pi(x, 0) = \Pi_0$, $0 \leq x \leq L$ must be satisfied. In region III, where the concentration is given by Eq. (24), we find

$$\Pi_3(x, t) = y(x) - \kappa C_s t e^{-\kappa x/v} \quad (27)$$

for some unknown function $y(x)$ that will be determined using the expression for the precipitate in the adjoining region II. An explicit formula $C_2(x, t)$ is not available here, but we can make the substitution $t = \tilde{t}_2(x, \lambda)$ in Eq. (26) and let $C_2(x, \tilde{t}_2(x, \lambda)) = \tilde{C}_2(x, \lambda)$, given by Eq. (22). Denoting the precipitate in these coordinates by $\tilde{\Pi}_2(x, \lambda)$, it may be shown that

$$\tilde{\Pi}_2(x, \lambda) = \kappa \int [\tilde{C}_2(x, \lambda) - C_s] \frac{d\tilde{t}_2}{d\lambda} d\lambda = p(x, \lambda) + q(x) \quad (28)$$

where the anti-derivative $p(x, \lambda)$ is

$$p(x, \lambda) = \frac{A}{B} \left[\frac{1}{1 + B\tilde{C}_2(x, \lambda)} - \frac{e^{-\kappa x/v}}{1 + \lambda BC_s} \right] \quad (29)$$

We now choose the arbitrary functions $y(x)$ and $q(x)$ in Eqs. (27) and (28) in such a way that the precipitate profile is always continuous. Thus, we need $\tilde{\Pi}_2(x, 1) = \Pi_0$, which determines $q(x) = \Pi_0 - p(x, 1)$ and hence

$$\tilde{\Pi}_2(x, \lambda) = \Pi_0 + \frac{A}{B} \left[\frac{1}{1 + B\tilde{C}_2(x, \lambda)} - \frac{1 + \lambda BC_s + BC_s - B\tilde{C}_2(x, \lambda)}{(1 + \lambda BC_s)(1 + BC_s)} \right] \quad (30)$$

Finally, by equating $\tilde{\Pi}_2(x, \lambda)$ and $\Pi_3(x, t)$ on the curve ℓ_0 separating regions II and III (see Fig. 6) we find

$$y(x) = \tilde{\Pi}_2(x, 0) + \tilde{t}_2(x, 0) \kappa C_s e^{-\kappa x/v} \quad (31)$$

Substituting this into Eq. (27) and cancelling terms then yields the following expression for the precipitate profile in region III:

$$\Pi_3(x, t) = \Pi_0 + C_s e^{-\kappa x/v} \left[\frac{\kappa x}{V_L(C_s)} - \kappa t + \Gamma_0' \ln(1 + BC_s - BC_s e^{-\kappa x/v}) \right] \quad (32)$$

Figure 8 visualises the surface described by Π_0 , $\tilde{\Pi}_2(x, \lambda)$ and $\Pi_3(x, t)$ on the domain $\{0 \leq x \leq L, t \leq t^*\} \subseteq \Omega$. It may be verified that $\tilde{\Pi}_2 > 0$ and $\Pi_3 \geq 0$ here, with $\Pi_3(x, t) = 0$ if and only if $x = 0, t = t^*$.

For a fixed value P , consider the level curve $(t, x_P(t), P)$ on the surface and its projection $(t, x_P(t))$ onto the x, t -plane, as indicated in Fig. 8. In region III, x_P satisfies $\Pi_3(x_P, t) = P$ and, denoting the corresponding concentration value $C_3(x_P)$ by C_P , the inverse function theorem can be used to show that

$$\frac{dx_P}{dt} = \frac{v(C_s - C_P)}{\Pi_0 - P + \frac{C_s - C_P}{C_s} \left[C_s + \frac{\Gamma_0}{1 + BC_P} \right]} \quad (33)$$

Equation (33) holds the key to the construction of the entire solution. It describes the velocity of a precipitate value P in terms of the corresponding concentration level C_P . It can be

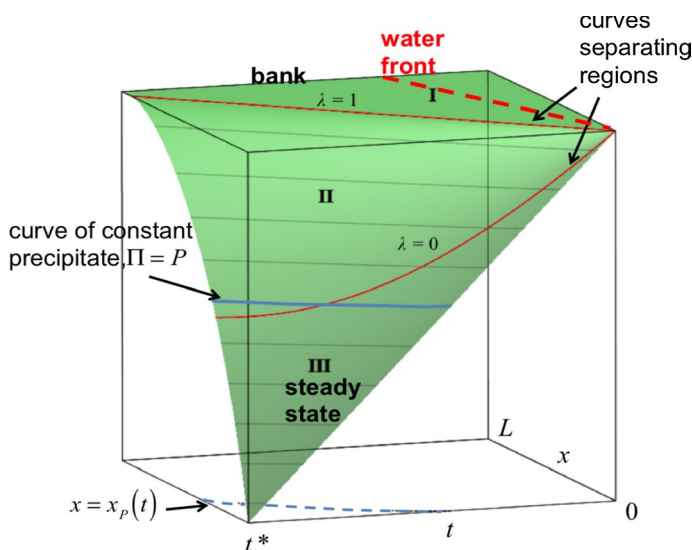


Fig. 8 Continuous precipitate surface corresponding to Fig. 7

verified that this relationship also holds in region II, with $C_p = C_2(x_p, t)$. A strictly mathematical proof of this fact is still at large, but it would probably involve the use of the chain rule in conjunction with the parametric solution components $\tilde{C}_2(x, \lambda)$, $\tilde{\Pi}_2(x, \lambda)$. Ideally, we would like to prove the stronger statement that Eq. (33) must apply to *any* new solution region which emerges, as long as the precipitate profile is required to be continuous. In the absence of a rigorous proof of this statement, we will henceforth *assume* that Eq. (33) is *invariant* between solution regions that are joined by a continuous precipitate profile.

4 Solution for $t \geq t^*$; Case 1: $\Pi_0 \geq BC_s \Gamma_0$

We now consider the time period after the precipitate “runs out” at the inlet; i.e. $t > t^*$. For this discussion, we will employ the curve $x = \alpha_{\Pi}(t)$ introduced in Sect. 2.2. With $\Pi_3(0, t^*) = 0$, Eq. (6) implies that $\partial \Pi / \partial t = 0$, which causes Eq. (5) to change its form to $\partial C / \partial t + V_L(C) \partial C / \partial x = 0$. Analogous to the argument given in Sorbie and Stamatiou (2018), it will be convenient to introduce also the point $\alpha_C = \alpha_C(t)$ such that $C \equiv 0$ for $x \leq \alpha_C$ and $C > 0$ for $x > \alpha_C$. Since $C \equiv 0$ is not a solution of Eq. (5) in Ω_+ , we must always have $\alpha_C \leq \alpha_{\Pi}$, which will effectively “slow down” the movement of α_C .

Note that $\alpha_{\Pi}(t^*) = \alpha_C(t^*) = 0$ and we consider the propagation speeds of the points α_{Π} and α_C to decide what is happening for $t > t^*$. In the case of α_C , we observe that $\Pi(\alpha_C, t) = 0$ since $\alpha_C \leq \alpha_{\Pi}$. The PDE $\partial C / \partial t + V_L(C) \partial C / \partial x = 0$ then implies that

$$\frac{d\alpha_C}{dt} = V_L(0) = \frac{v}{1+A} \quad (34)$$

For the motion of α_{Π} , we use the assumed invariance of Eq. (33) between solution regions. Thus, for $t \geq t^*$, we suppose that

$$\frac{d\alpha_{\Pi}}{dt} = \frac{vC_s - vC(\alpha_{\Pi}, t)}{\Pi_0 + \frac{C_s - C(\alpha_{\Pi}, t)}{C_s} \left[1 + \frac{\Gamma_0}{1 + BC(\alpha_{\Pi}, t)} \right]}, \quad t \geq t^* \quad (35)$$

In particular, $C(\alpha_{\Pi}, t^*) = C(\alpha_C, t^*) = 0$ and hence

$$\left. \frac{d\alpha_{\Pi}}{dt} \right|_{t=t^*} = \frac{vC_s}{\Pi_0 + C_s + \Gamma_0} \quad (36)$$

Comparing Eqs. (34) and (36), we see that

$$\left. \frac{d\alpha_{\Pi}}{dt} \right|_{t=t^*} \leq \left. \frac{d\alpha_C}{dt} \right|_{t=t^*} \Leftrightarrow \Pi_0 \geq BC_s \Gamma_0 \quad (37)$$

Let us now suppose that $\Pi_0 \geq BC_s \Gamma_0$ (Case 1). Together with the constraint $\alpha_C \leq \alpha_{\Pi}$, this implies the emergence of a *joint root* $x_0 = \alpha_{\Pi} = \alpha_C$ for all $t \geq t^*$ moving at constant velocity $U_1 := vC_s(\Pi_0 + C_s + \Gamma_0)^{-1}$ [let $C(\alpha_{\Pi}, t) = 0$ in Eq. (35)]. This suggests there is some new region in Ω , next to region III, in which the concentration and precipitate components are given by travelling wave solutions. To specify these solutions, let $z = x - U_1 t$ and $C = c(z)$ in Eq. (5). This yields the ODE

$$\frac{dc}{dz} = \frac{\kappa(C_s - c)}{v - U_1 - \Gamma_{eq}'(c)} \quad (38)$$

Equation (38) may be solved to give z up to an arbitrary constant η_1 :

$$z = \frac{U_1 - v}{\kappa} \ln(C_s - c) + \frac{U_1 \Gamma_0}{\kappa C_s} \frac{1}{1 + Bc} + \frac{U_1 \Gamma_0'}{\kappa} \ln\left(\frac{C_s - c}{1 + Bc}\right) + \eta_1 \quad (39)$$

Putting back $z = x - U_1 t$ and using the condition that $c = 0$ at $x_0 = U_1(t - t^*)$, we determine the constant

$$\eta_1 = -U_1 t^* - \frac{U_1 - v}{\kappa} \ln(C_s) - \frac{U_1 \Gamma_0}{\kappa C_s} - \frac{U_1 \Gamma_0'}{\kappa} \ln(C_s) \quad (40)$$

Then, the new solution component, C_4 say, is implicitly defined as follows:

$$x + \frac{v}{\kappa} \ln\left(\frac{C_s - c}{C_s}\right) = U_1(t - t^*) + \frac{vU_1}{\kappa V_L(C_s)} \ln\left(\frac{C_s - c}{C_s}\right) - \frac{U_1 \Gamma_0'}{\kappa} \ln(1 + Bc) + \frac{U_1 \Gamma_0}{\kappa C_s} \left[\frac{1}{1 + Bc} - 1 \right] \quad (41)$$

To determine region IV in which Eq. (41) applies, we consider its intersection with Eq. (25). Substituting $c = C_3(x)$ into Eq. (41) and dividing by U_1 , we obtain

$$t = t^* + \frac{x}{V_L(C_s)} + \frac{\Gamma_0'}{\kappa} \ln(1 + BC_3(x)) + \frac{\Gamma_0}{\kappa C_s} \left[1 - \frac{1}{1 + BC_3(x)} \right] \quad (42)$$

We recognise Eq. (42) as the characteristic $t = \tilde{t}_3(x, r_{TW})$ with parameter value r_{TW} defined by the relation

$$t^* = \tilde{t}_3(0, r_{TW}) = \frac{-r_{TW}}{V_L(C_s)} - \frac{\Gamma_0'}{\kappa} \ln(1 + BC_3(r_{TW})) + \frac{\Gamma_0}{\kappa C_s} \left[\frac{1}{1 + BC_3(r_{TW})} - 1 \right] \quad (43)$$

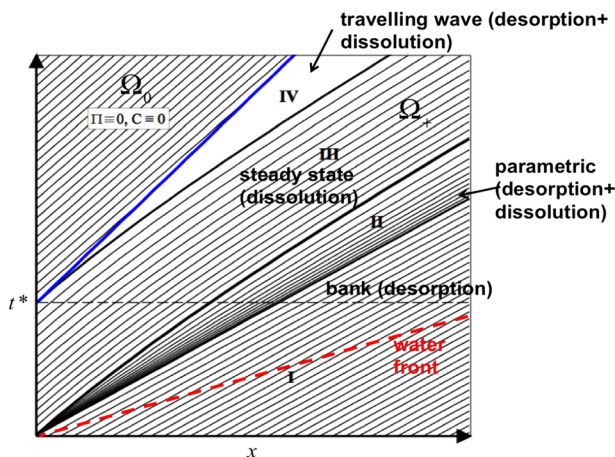
Figure 9 shows region IV bounded by the (blue) line $x_0 = U_1(t - t^*)$ and the characteristic projection $t = \tilde{t}_3(x, r_{TW})$ emanating from $t = t^*$. The characteristics in region IV are not shown, but it is possible to obtain them by using a different parameterisation of the Cauchy problem in which $s = 0$ on the curve $x_0 = U_1(t - t^*)$ instead of at $t = 0$. The condition $C(x_0) = 0$ then translates into an equivalent condition in terms of r , enabling us to determine the (new) function $f(r)$.

Note that, for a fixed concentration value c , Eq. (41) describes its path in region IV. The initial position of c (in region III) is $X_c := -v\kappa^{-1} \ln(1 - c/C_s)$ and its velocity is U_1 for $t \geq T_c := \tilde{t}_3(X_c, r_{TW})$. This observation can also be used to construct Π_4 : the precipitate value corresponding to c is $P_c := \Pi_3(X_c, T_c)$ and the paths traced out by c and P_c in the x, t -plane coincide for $t \geq T_c$.

In summary, if $\Pi_0 \geq BC_s\Gamma_0$, the solution in Ω_+ consists of four regions I, II, III and IV in which the concentration is given by the components C_s , \tilde{C}_2 , C_3 and C_4 , respectively. Region I is due to adsorption and region III due to dissolution, whereas both mechanisms are active in regions II and IV. In Ω_0 , Eq. (5) becomes $\partial C/\partial t + V_L(C)\partial C/\partial x = 0$, describing the case of pure adsorption/desorption. The characteristics here are straight lines of slope $V_L(0) > U_1$, determined by the data $C(0, t) = 0$, and they run into the moving boundary $x_0 = U_1(t - t^*)$.

Example 1 This Case 1 ($\Pi_0 \geq BC_s\Gamma_0$) solution is illustrated by a numerical example. Let $A = 1, B = 10, C_s = 0.1, v = 1, \kappa = 1, L = 1$. We then calculate $\Gamma_0 = \Gamma_{eq}(C_s) = 0.05$ and the Langmuir velocities $V_L(0) = 0.5$, $V_L(C_s) = 0.8$. Note that $BC_s\Gamma_0 = 0.05$, so Case 1 (just) occurs if we choose $\Pi_0 = 0.05$. Figure 10 shows the solution profiles consisting of C_1, \tilde{C}_2, C_3 and $\Pi_1, \tilde{\Pi}_2, \Pi_3$ at $t = t^* = 0.5$, with the adsorption curve plotted in red. Since $\Pi_0 = BC_s\Gamma_0$, we have $\alpha'_{\Pi}(t^*) = V_L(0)$ and the travelling wave solution component emerges with this speed (see Fig. 11). We observe that $\partial C/\partial x = \infty$ at $x = \alpha_{\Pi} = V_L(0)t$, which is a

Fig. 9 Solution regions and characteristic projections for Case 1 ($\Pi_0 \geq BC_s\Gamma_0$)



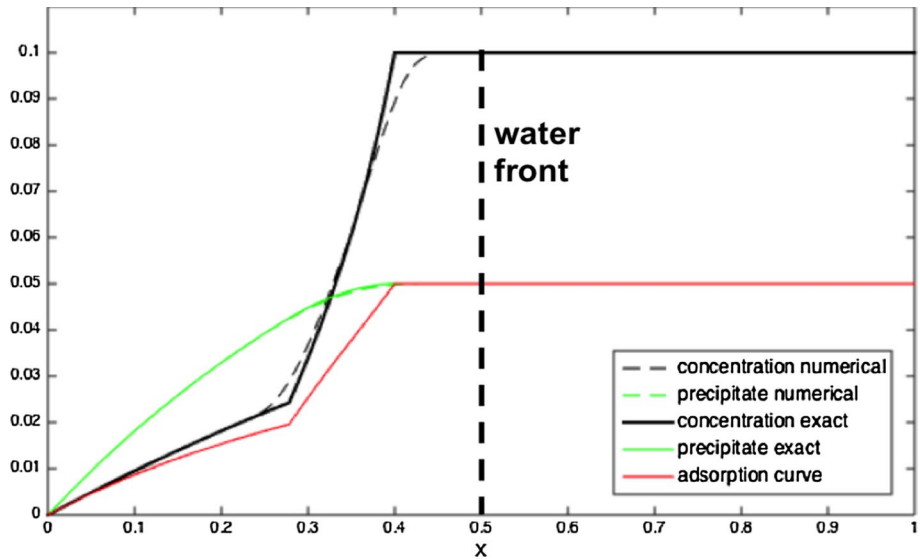


Fig. 10 Solution profiles of Example 1 at $t = t^* = 0.5$

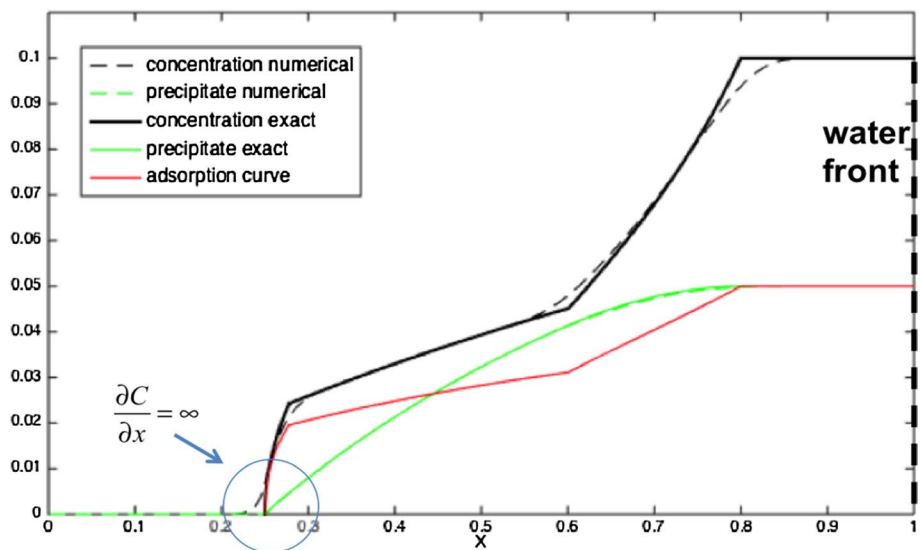


Fig. 11 Solution profiles of Example 1 at $t = 1 > t^*$

result of the tangency of the boundary curve and the characteristic $t = \tilde{t}_3(x, r_{TW})$ at $(0, t^*)$. This blow-up is also visible in the effluent concentration plot in Fig. 12. Note that a larger value of Π_0 would result in a lower travelling wave speed and a more horizontal solution component, the derivative remaining finite everywhere. On the other hand, a lower value of Π_0 leads to qualitatively different solution (see Case 2 below).

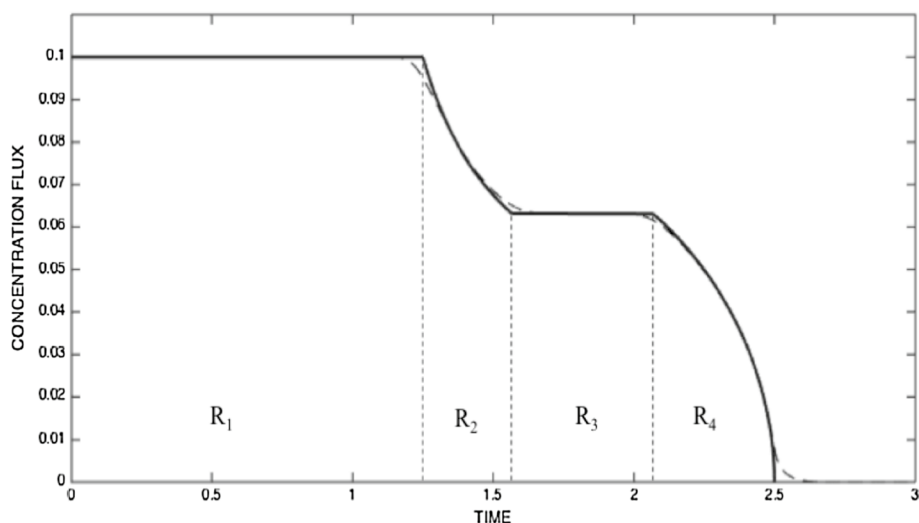


Fig. 12 Concentration flux at $x = L$ for Example 1

The effluent concentration flux can be used to prove explicitly that our constructed solution conserves the total amount of chemical present in the system. The profile can be divided into four parts from left to right, as shown in Fig. 12. Here, we have

$$R_1 = v C_s \tilde{t}_2(L, 1) = C_s L (1 + \Gamma_0') \quad (44)$$

And, defining the constant $\mu := \tilde{C}_2(L, 0) = C_s - C_s e^{-\kappa L/v}$, we compute

$$\begin{aligned} R_2 &= \int_{\lambda=1}^{\lambda=0} v \cdot \tilde{C}_2(L, \lambda) \cdot \frac{d}{d\lambda} \tilde{t}_2(L, \lambda) d\lambda \\ &= \frac{v}{\kappa} \left[\frac{\Gamma_0 B \mu^2}{C_s (1 + B\mu)} + C_s \Gamma_0' \ln(1 + B\mu) \right] \end{aligned} \quad (45)$$

Furthermore, denoting Eq. (41) as $t = t_{TW}(x, c)$, observe that

$$R_3 + R_4 = \int_0^{v\mu} t_{TW}(L, c) dc - v\mu \tilde{t}_2(L, 0) \quad (46)$$

The integral on the right hand side evaluates to

$$\begin{aligned} \int_0^{v\mu} t_{TW}(L, c) dC &= \frac{v}{\kappa} \Gamma_0' (\mu - C_s) \ln(1 + B\mu) \\ &\quad + \Gamma_0' L (\mu - C_s) + L (\Pi_0 + \mu + \Gamma_0) \end{aligned} \quad (47)$$

and, from Eq. (23),

$$-v\mu \tilde{t}_2(L, 0) = \frac{v}{\kappa} \left[\frac{\Gamma_0 \mu}{C_s(1+B\mu)} - \frac{\Gamma_0}{C_s} \mu - \Gamma_0' \mu \ln(1+B\mu) \right] - L(1+\Gamma_0')\mu \quad (48)$$

Finally, combining Eqs. (44)–(48), we find that

$$\sum_{i=1}^4 R_i = L(\Pi_0 + C_s + \Gamma_0) \quad (49)$$

This is exactly the amount of scale inhibitor initially present in the system.

5 Solution for $t \geq t^*$; Case 2: $\Pi_0 < BC_s\Gamma_0$

With $\Pi_0 < BC_s\Gamma_0$, we have $\alpha_{\Pi}'(t^*) > V_L(0)$ and, during some time interval after t^* , the boundary curve $x = \alpha_{\Pi}(t)$ (see Sect. 2.2) is defined by $\Pi_3(\alpha_{\Pi}, t) = 0$ [Eq. (32)]. Its slope, $V_{\Pi} = d\alpha_{\Pi}/dt$, is then given by Eq. (35) with $C(\alpha_{\Pi}, t) = C_3(\alpha_{\Pi})$. For the purpose of the following discussion, we will let $y = C_3(\alpha_{\Pi})$, so that

$$\alpha_{\Pi} = C_3^{-1}(y) = -\frac{v}{\kappa} \ln \left(\frac{C_s - y}{C_s} \right) \quad (50)$$

Note that, in terms of y , the equation $\Pi_3(\alpha_{\Pi}, t) = 0$ can be re-written as $t = t_{\Pi 3}(y)$, where the function $t_{\Pi 3} : \mathbb{R} \rightarrow \mathbb{R}$ is

$$t_{\Pi 3}(y) := \frac{1}{\kappa} \left[\frac{\Pi_0}{C_s - y} + \Gamma_0' \ln(1 + By) - \frac{v}{V_L(C_s)} \ln \left(\frac{C_s - y}{C_s} \right) \right] \quad (51)$$

Furthermore, we define the function $T_3 : \mathbb{R} \rightarrow \mathbb{R}$ by evaluating $\tilde{t}_3(x, r = 0)$ (or, equivalently, $\tilde{t}_2(x, \lambda = 0)$) at $x = \alpha_{\Pi} = C_3^{-1}(y)$, so

$$\begin{aligned} T_3(y) &:= \tilde{t}_3(C_3^{-1}(y), 0) \\ &= \frac{1}{\kappa} \left[-\frac{v}{V_L(C_s)} \ln \left(\frac{C_s - y}{C_s} \right) + \Gamma_0' \ln(1 + By) + \frac{\Gamma_0}{C_s} \frac{By}{1 + By} \right] \end{aligned} \quad (52)$$

Finally, we also consider $V_{\Pi} = d\alpha_{\Pi}/dt$ in terms of y :

$$V_{\Pi}(y) = \frac{v(C_s - y)}{\Pi_0 + \frac{C_s - y}{C_s} \left[C_s + \frac{\Gamma_0}{1 + By} \right]} \quad (53)$$

This will describe $d\alpha_{\Pi}/dt$ until y is the *minimum* of the following two values:

- (a) $\xi_a \in [0, C_s]$ such that $V_{\Pi}(\xi_a) = V_L(\xi_a)$ and $V_{\Pi}(y) > V_L(y)$ for all $y \in [0, \xi_a)$
- (b) $\xi_b \in [0, C_s]$ such that $t_{\Pi 3}(\xi_b) = T_3(\xi_b)$ and $t_{\Pi 3}(y) > T_3(y)$ for all $y \in [0, \xi_b)$

Note that $V_{\Pi}(0) > V_L(0)$ and $t_{\Pi 3}(0) = t^* > 0 = T_3(0)$. We will now determine the values ξ_a , ξ_b and establish when $\xi_a \leq \xi_b$ and $\xi_a > \xi_b$. From Eqs. (9) and (53), it follows that

$$V_{\Pi}(y) = V_L(y) \quad \Leftrightarrow \quad \left(\frac{C_s - y}{1 + By} \right)^2 = \frac{\Pi_0 C_s}{B\Gamma_0} \quad (54)$$

The quadratic on the right hand side has roots

$$y_a^{\pm} = \frac{\Pi_0 + \Gamma_0 \pm (1 + BC_s) \sqrt{\frac{\Pi_0 \Gamma_0}{BC_s}}}{\frac{\Gamma_0}{C_s} - B\Pi_0} \quad (55)$$

Furthermore, it can be shown that

$$\frac{dV_{\Pi}}{dy} = \frac{V_{\Pi}(y) - V_L(y)}{V_L(y)} \quad (56)$$

Since $V_{\Pi}(0) > V_L(0)$, we have $V'_{\Pi}(0) > 0$. From Eq. (53), we deduce that $V_{\Pi}(0) > V_{\Pi}(C_s) = 0$ and that V_{Π} is continuous on $[0, C_s]$. It then follows that V_{Π} has a maximum on $[0, C_s]$ and, by Eq. (56), $V_L = V_{\Pi}$ here. In order to determine whether this point is y_a^- or y_a^+ , we write $\Pi_0 = (1 + \varepsilon)^2 B^{-1} C_s^{-1} \Gamma_0$ for some $\varepsilon \in \mathbb{R}$. If $\varepsilon > 0$, the denominator in Eq. (55) is negative and $y_a^+ < 0$. The above argument now guarantees that $y_a^- \in [0, C_s]$. With $\varepsilon < 0$, the denominator is positive and we need to examine whether $y_a^- \geq 0$ or $y_a^- < 0$. Substituting for Π_0 in the numerator, we find

$$\begin{aligned} \Gamma_0 \left[\frac{(1 + \varepsilon)^2}{BC_s} + 1 - \frac{1 + BC_s}{BC_s} (1 + \varepsilon) \right] &= \frac{\Gamma_0}{BC_s} [(1 + \varepsilon)^2 + BC_s - (1 + BC_s)(1 + \varepsilon)] \\ &= \frac{\Gamma_0}{BC_s} \varepsilon (1 + \varepsilon - BC_s) \end{aligned} \quad (57)$$

By assumption of Case 2, we also have $BC_s \Gamma_0 > \Pi_0 = (1 + \varepsilon)^2 B^{-1} C_s^{-1} \Gamma_0$. Hence, $1 + \varepsilon < BC_s$ and $y_a^- > 0$. Moreover, since $y_a^- < y_a^+$, it must be that $y_a^- \in [0, C_s]$. Finally, if the denominator in Eq. (55) is zero (i.e. $\varepsilon = 0$), we can take the limit $\varepsilon \rightarrow 0$ to find $y_a^- = (BC_s - 1)/2B > 0$, while the other root y_a^+ is undefined. Thus, for all parameter choices satisfying $\Pi_0 < BC_s \Gamma_0$, y_a^- is the lowest value such that $V_{\Pi} = V_L$ and we write $\xi_a = y_a^-$ (see Fig. 13).

We need to compare $\xi_a = y_a^-$ with the solutions of the equation $t_{\Pi 3}(y) = T_3(y)$. From Eqs. (51) and (52), it follows that

$$T_3(y) \leq t_{\Pi 3}(y) \quad \Leftrightarrow \quad \frac{y(C_s - y)}{1 + By} \leq \frac{\Pi_0 C_s}{B\Gamma_0} \quad \Leftrightarrow \quad y \leq y_b^- \text{ or } y \geq y_b^+ \quad (58)$$

where equality/inequality occur simultaneously and

$$y_b^{\pm} = \frac{BC_s(\Gamma_0 - \Pi_0) \pm \sqrt{D}}{2B\Gamma_0} \quad (59)$$

The discriminant is $D = B^2 C_s^2 (\Gamma_0 - \Pi_0)^2 - 4BC_s \Gamma_0 \Pi_0$, and we have

$$D = 0 \quad \Leftrightarrow \quad \Pi_0 = \beta^{\pm} = \Gamma_0 + \frac{2\Gamma_0}{BC_s} \left(1 \pm \sqrt{1 + BC_s} \right) \quad (60)$$

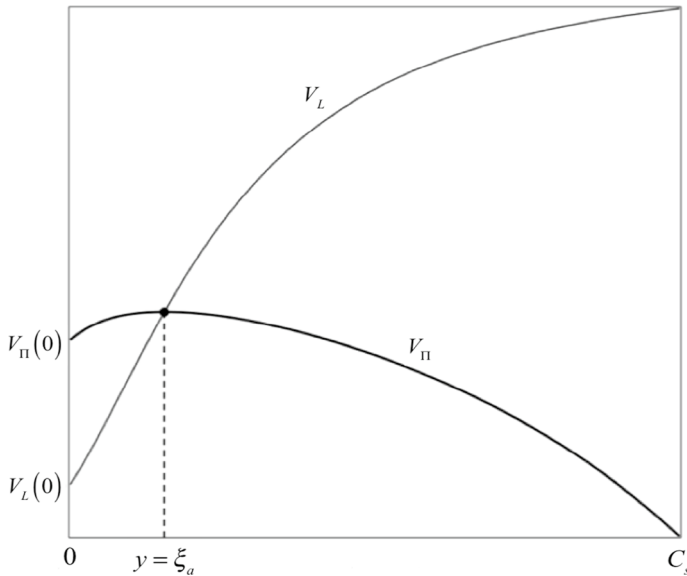


Fig. 13 The curves V_{Π} and V_L meet at $y = \xi_a = y_a^-$, given by Eq. (55)

Moreover, $D > 0$ if and only if $\Pi_0 < \beta^-$ or $\Pi_0 > \beta^+$. But, $\Pi_0 > \beta^+$ implies that $\Pi_0 > \Gamma_0$ and hence $y_b^- < y_b^+ < 0$. In this case, it follows from Eq. (58) that $t_{\Pi 3}(y) > T_3(y)$ for all $y \in [0, C_s]$. The same is true if $D < 0$. Thus, for all parameter choices satisfying $\Pi_0 > \beta^-$, there is no ξ_b such that $t_{\Pi 3}(\xi_b) = T_3(\xi_b)$.

Now suppose that $\Pi_0 \leq \beta^-$. Then, $\Pi_0 < \Gamma_0$ and we have $0 < y_b^- < y_b^+ < C_s$. It may be verified that

$$\Pi_0 = \beta^- \Rightarrow y_a^- = y_b^- = F := \frac{\sqrt{1 + BC_s} - 1}{B} \quad (61)$$

For this particular choice of parameters, $V_{\Pi} = d\alpha_{\Pi}/dt$ is equal to the Langmuir velocity of $y = C_3(\alpha_{\Pi})$ exactly at the time that solution region III disappears, i.e. when the boundary curve $x = \alpha_{\Pi}(t)$ enters region II. Since $D = 0$, the boundary curve is tangent to the characteristic curve $t = \tilde{\tau}_3(x, 0)$ at the point $x_a = C_3^{-1}(y_a^-)$, $\tau_a = t_{\Pi 3}(y_a^-)$ (see Fig. 14).

If $\Pi_0 < \beta^-$ we have

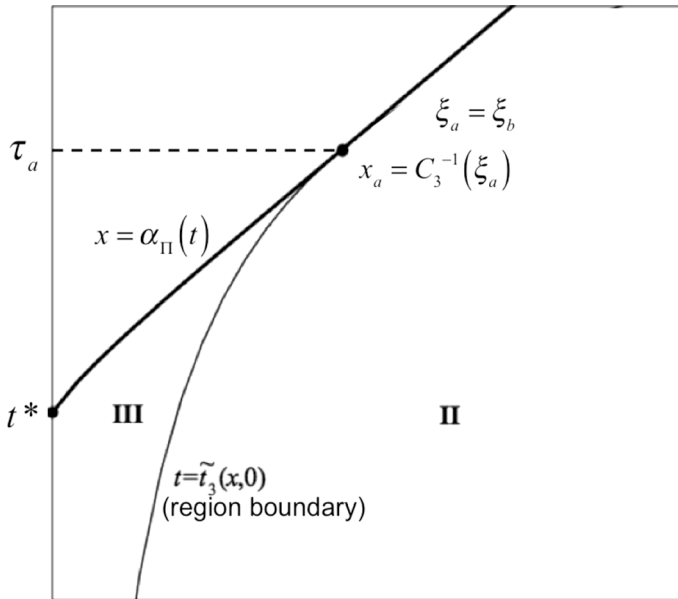


Fig. 14 When $\Pi_0 = \beta^-$ [Eq. (60)], we have $\xi_a = \xi_b$

$$\begin{aligned}
 \frac{\Pi_0 C_s}{B\Gamma_0} &< \frac{BC_s + 2(1 - \sqrt{1 + BC_s})}{B^2} \\
 &= \left(\frac{\sqrt{1 + BC_s} - 1}{B} \right)^2 \\
 &= \left(\frac{1 + BC_s - \sqrt{1 + BC_s}}{B\sqrt{1 + BC_s}} \right)^2 \\
 &= \left(\frac{C_s - F}{1 + BF} \right)^2
 \end{aligned} \tag{62}$$

Since y_a^- satisfies Eq. (54), it must be that $y_a^- > F$, which is equivalent to

$$y_a^- > \frac{C_s - y_a^-}{1 + B y_a^-} \tag{63}$$

Finally, this and Eq. (58) imply that

$$y_a^- \left(\frac{C_s - y_a^-}{1 + B y_a^-} \right) > \left(\frac{C_s - y_a^-}{1 + B y_a^-} \right)^2 = \frac{\Pi_0 C_s}{B\Gamma_0} \Rightarrow T_3(y_a^-) > t_{\Pi 3}(y_a^-) \tag{64}$$

Since $t_{\Pi 3}(0) > T_3(0)$ and $t_{\Pi 3}, T_3$ are continuous on $[0, C_s]$, the curves $t = t_{\Pi 3}(y)$ and $t = T_3(y)$ intersect on $(0, y_a^-)$ and we must have $0 < y_b^- < y_a^- \leq y_b^+$.

In summary, if $\Pi_0 > \beta^-$, then ξ_b does not exist. Region III continues to exist for all time and we have $\xi_a = y_a^-$. Define $\tau_a := t_{\Pi 3}(\xi_a)$ and $x_a := C_3^{-1}(\xi_a)$. The boundary curve $x = \alpha_{\Pi}(t)$

now lies above the characteristic $t = \tilde{t}_3(x, 0)$ in the x, t -plane and $V_{\Pi} = d\alpha_{\Pi}/dt$ varies according to Eq. (35) with $y = C_3(\alpha_{\Pi}, t)$ until $t = \tau_a$. We will refer to this scenario as *Case 2a*. It is to be distinguished from *Case 2b*, which occurs if $\Pi_0 \leq \beta^-$. The boundary curve then intersects with the characteristic at the point $x_b := C_3^{-1}(\xi_b)$, $\tau_b := t_{\Pi 3}(\xi_b)$, where $\xi_b = y_b^- < \xi_a$. At time $t = \tau_b$, solution region III disappears and for $t \geq \tau_b$, the motion of α_{Π} is determined by the parametric solution in region II. By assumption of the invariance of Eq. (33), the velocity $V_{\Pi} = d\alpha_{\Pi}/dt$ is now given by Eq. (35) with $y = C_2(\alpha_{\Pi}(\lambda), \lambda)$. We can therefore still expect to have $V_{\Pi} = V_L$ when $y = \xi_a = y_a^-$. This will be verified in terms of the auxiliary parameter λ in Sect. 5.2.

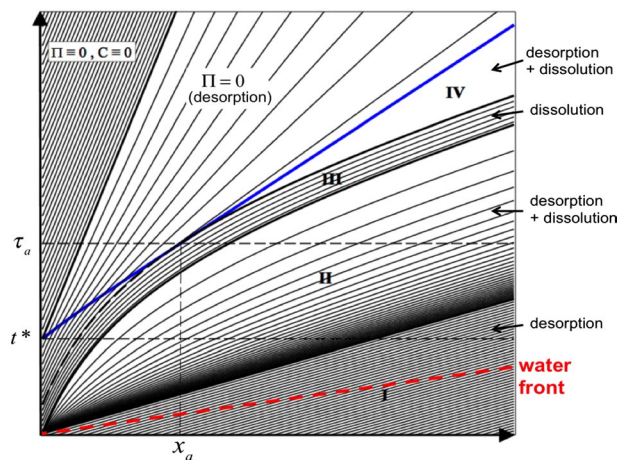
5.1 Solution for Case 2a: $\Pi_0 > \beta^-$

For $t > \tau_a$, we have $C(\alpha_{\Pi}, t) = \xi_a$, which is the concentration level “supplied” by the pure adsorption solution on $0 < x < \alpha_{\Pi}(t)$. Using the invariance of Eq. (33), we consider the constant velocity $U_2 := V_{\Pi}(\xi_a) = V_L(\xi_a)$ and look for a travelling wave solution of Eq. (5) in Ω_+ . Such a solution is of the form of Eq. (39) with U_1, η_1 replaced by U_2, η_2 . The constant of integration, η_2 , is now determined by the condition that $c = \xi_a$ at $x = \alpha_{\Pi}(t) = x_a + U_2(t - \tau_a)$. We then obtain the solution

$$x = U_2(t - \tau_a) + \frac{U_2 x_a}{V_L(C_s)} + \left(\frac{U_2}{V_L(C_s)} - 1 \right) \frac{v}{\kappa} \ln \left(\frac{C_s - c}{C_s} \right) - \frac{U_2 \Gamma_0'}{\kappa} \ln \left(\frac{1 + Bc}{1 + B\xi_a} \right) + \frac{U_2 \Gamma_0}{\kappa C_s} \left[\frac{1}{1 + Bc} - \frac{1}{1 + B\xi_a} \right] \quad (65)$$

Substituting $c = C_3(x)$ and dividing by U_2 , it may be verified that, for $t > \tau_a$, the travelling wave solution intersects with component C_3 along the characteristic $t = \tilde{t}_3(x, r_{TW2})$, where the parameter value r_{TW2} is defined by $\tau_a = \tilde{t}_3(x_a, r_{TW2})$. This curve and the line $x = x_a + U_2(t - \tau_a)$ enclose the new solution region IV, as shown in Fig. 15. The characteristics in this region are not shown, but may be obtained as described for Case 1. The boundary curve $x = \alpha_{\Pi}(t)$ is plotted in blue, and the characteristic $t = \tilde{t}_3(x, r_{TW2})$ is tangent

Fig. 15 Solution regions in Case 2a ($\Pi_0 > \beta^-$)



to this curve at (x_a, τ_a) . As mentioned before, the motion of α_{Π} for $t^* \leq t \leq \tau_a$ also results in a pure adsorption/desorption solution in Ω_0 :

$$x = -\frac{v}{\kappa} \ln \left(\frac{C_s - c}{C_s} \right) + V_L(c) \cdot (t - t_{\Pi 3}(c)) \quad (66)$$

Equation (66) describes the path of a concentration value $c \in [0, \xi_a]$. This lies at $x = -v\kappa^{-1} \ln(1 - c/C_s)$ in region III until $t = t_{\Pi 3}(c)$, when $c = C_3(\alpha_{\Pi})$. For $t \geq t_{\Pi 3}(c)$, c moves at its own Langmuir velocity $V_L(c)$. In Fig. 15, it is illustrated how a characteristic emanates from each point on the boundary curve between $(0, t^*)$ and (x_a, τ_a) . The effluent concentration flux for Case 2a consists of five regions (see Fig. 19 in Example 2) and can be used to prove that the solution satisfies mass balance, as was done for Case 1.

Example 2 Let $C_s = 0.1, v = 1, \kappa = 1, L = 1$ as before and choose $A = 10, B = 100$. We compute $\Gamma_0 = 0.0909$, $BC_s\Gamma_0 = 0.909$ and $\beta^- = 0.049$, so Case 2a occurs if we let $\Pi_0 = C_s = 0.1$. With $V_L(0) = 0.0909$ and $V_L(C_s) = 0.9237$ now, there is a much greater range of Langmuir velocity than in Example 1. This stretches the components \tilde{C}_2 and $\tilde{\Pi}_2$, which can be seen in the plot at $t = t^* = 1$ in Fig. 16 between $x = 0.2535$ and $x = 0.9237$. Equation (55) yields $\xi_a = y_a^- = 0.01548$ and hence $x_a = C_3^{-1}(\xi_a) = 0.1682$, $\tau_a = t_{\Pi 3}(\xi_a) = 1.443$. Figures 17 and 18 show the solution profiles at $t = \tau_a$ and $t = 2.5 > \tau_a$, respectively. The travelling wave solution component C_4 emerges at $t = \tau_a$ and lies between $x = 0.5845$ and $x = 0.8591$ in Fig. 18. Its speed is $U_2 = V_L(\xi_a) = 0.3937$. Component C_3 is always present, which is more apparent in the effluent concentration flux plotted in Fig. 19.

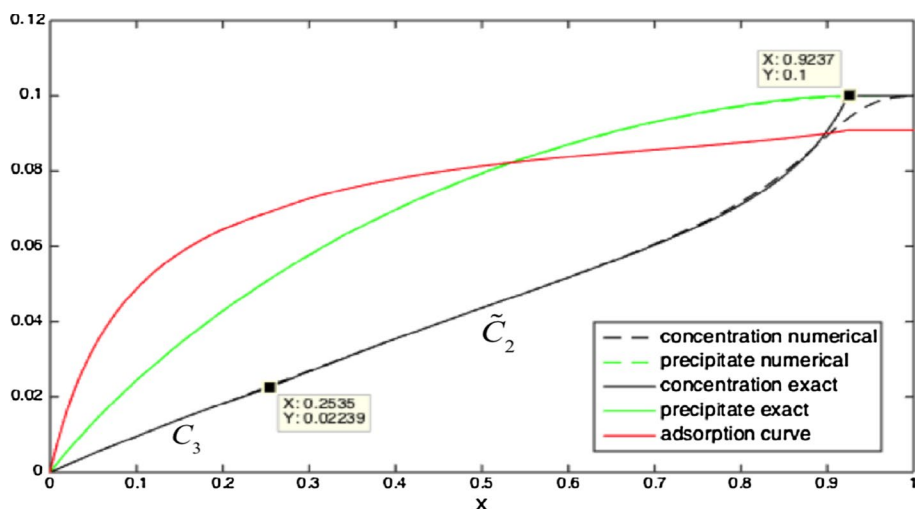


Fig. 16 Solution profiles of Example 2 at $t = t^* = 1$

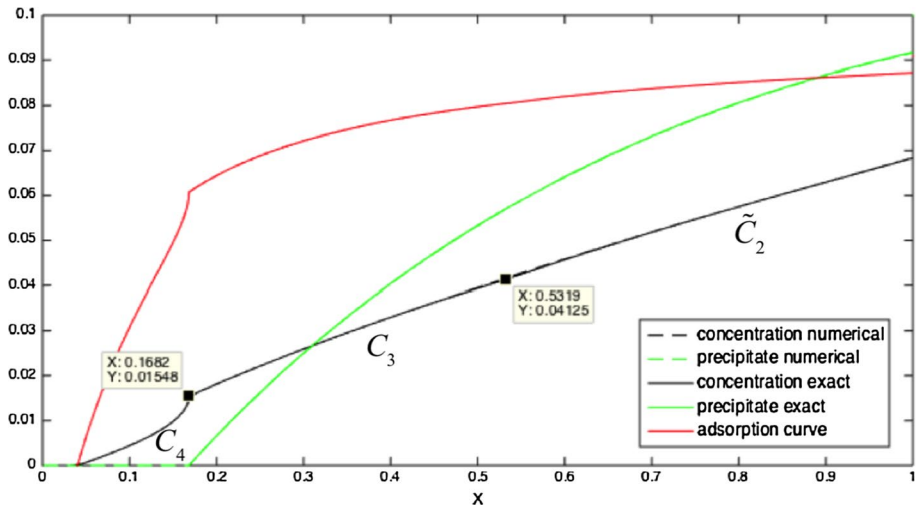


Fig. 17 Solution profiles of Example 2 at $t = \tau_a = 1.443 > t^*$

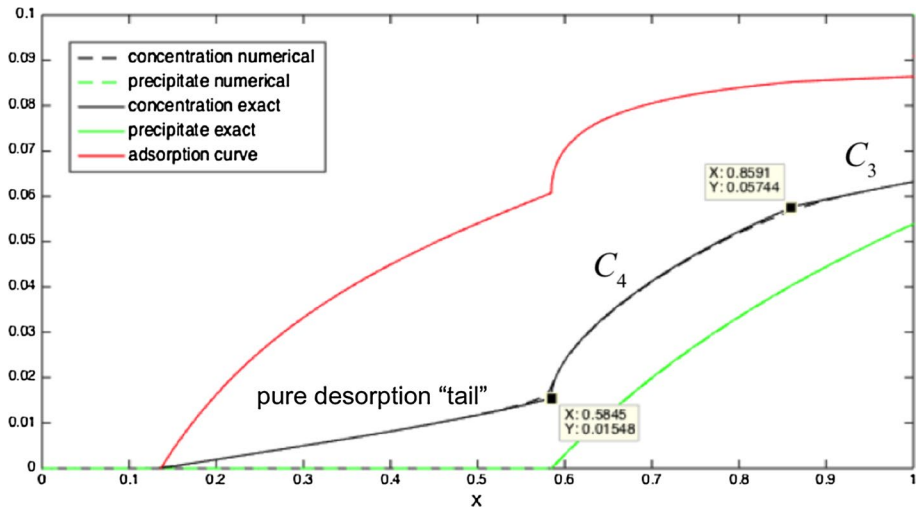


Fig. 18 Solution profiles of Example 2 at $t = 2.5 > \tau_a$

5.2 Solution for Case 2b: $\Pi_0 \leq \beta^-$

The characteristic $t = \tilde{\tau}_3(x, 0) = \tilde{\tau}_2(x, 0)$ now intersects the boundary curve $x = \alpha_\Pi(t)$ at (x_b, τ_b) , and region III disappears (see Fig. 20). For $t > \tau_b$, the boundary is determined by the solution in region II and can be found in terms of the auxiliary parameter $\lambda \in [0, 1]$, using the equation $\tilde{\Pi}_2(\alpha_\Pi, \lambda) = 0$.

Noticing that $t = \tilde{\tau}_2(x, \lambda)$ and employing the chain rule, we can determine the velocity of α_Π in terms of λ as follows:

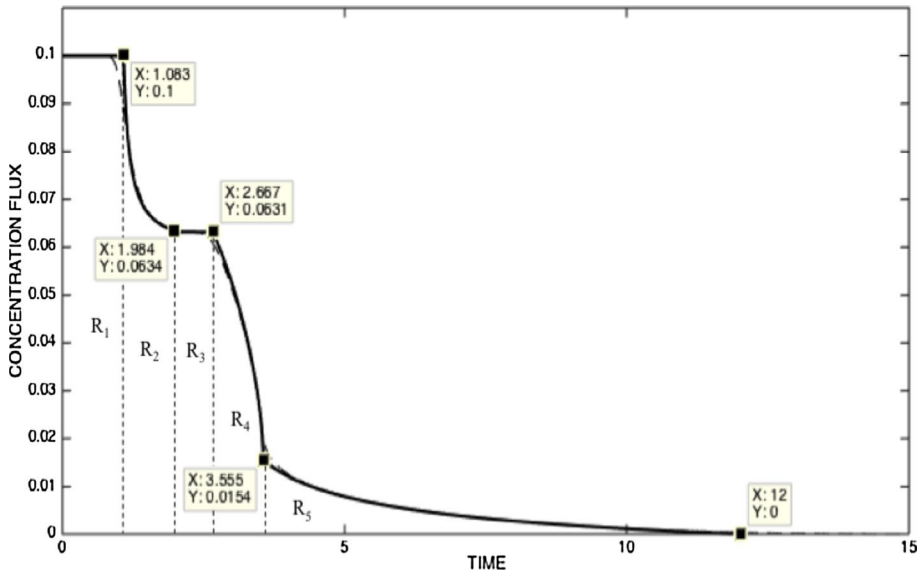
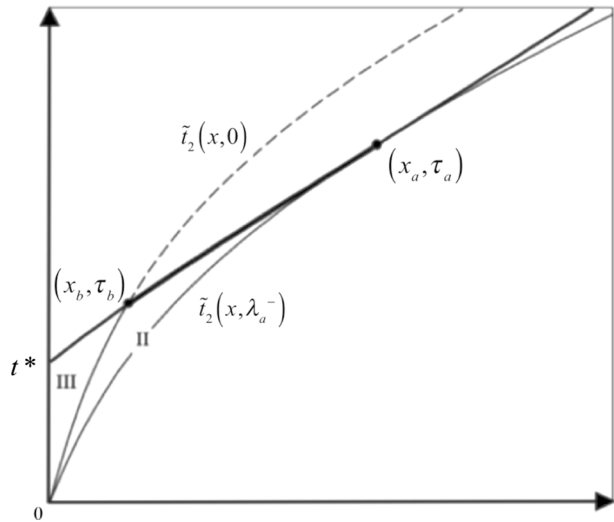


Fig. 19 Effluent concentration flux for Example 2

Fig. 20 If $\Pi_0 < \beta^-$, then $\xi_b < \xi_a$



$$V_{\Pi}(\lambda) = \frac{d}{dt} \alpha_{\Pi}(\lambda) = \frac{d\lambda}{dt} \frac{d\alpha_{\Pi}}{d\lambda} = \left(\frac{d}{d\lambda} \tilde{t}_2(\alpha_{\Pi}(\lambda), \lambda) \right)^{-1} \frac{d\alpha_{\Pi}}{d\lambda} \quad (67)$$

The concentration value at $x = \alpha_{\Pi}(\lambda)$ is $\tilde{C}_2(\alpha_{\Pi}(\lambda), \lambda)$, and we want to find out when $V_{\Pi}(\lambda) = V_L(\tilde{C}_2(\alpha_{\Pi}, \lambda))$. To simplify this analysis, we introduce

$$F(\lambda) := \frac{BC_s \Pi_0}{\Gamma_0} (1 + \lambda BC_s) - (1 + \lambda) BC_s \quad (68)$$

$$G(\lambda) := \frac{4BC_s\Pi_0}{\Gamma_0}(1 + \lambda BC_s) + 4\lambda B^2 C_s^2 \quad (69)$$

In terms of F and G , the solution $\alpha_\Pi(\lambda)$ of $\tilde{\Pi}_2(\alpha_\Pi, \lambda) = 0$ satisfies

$$\tilde{C}_2(\alpha_\Pi, \lambda) = \frac{-F(\lambda) \pm \sqrt{F(\lambda)^2 - G(\lambda)}}{2B} \quad (70)$$

Clearly, we need to have $0 \leq \tilde{C}_2(\alpha_\Pi(\lambda), \lambda) \leq C_s$ for $\lambda \in [0, 1]$. Observe that $G(\lambda) > 0$, which implies that both roots are negative if $F(\lambda) > 0$ and the equation $\tilde{\Pi}_2(\alpha_\Pi, \lambda) = 0$ has no meaningful solutions. On the other hand, if $F(\lambda) < 0$, then both roots are positive and we can restrict attention to the smaller root (corresponding to the negative sign), because the solution components \tilde{C}_2 and $\tilde{\Pi}_2$ are both decreasing in the x -direction and the t -direction (see Figs. 7, 8). Using Eq. (22) for \tilde{C}_2 , we then re-write Eq. (70) to obtain

$$\alpha_\Pi(\lambda) = -\frac{\nu}{\kappa} \ln \left(\frac{2BC_s + F(\lambda) + \sqrt{F(\lambda)^2 - G(\lambda)}}{2BC_s(1 - \lambda)} \right) \quad (71)$$

The roots of the discriminant $D = F(\lambda)^2 - G(\lambda)$ are

$$\lambda_a^\pm = \frac{BC_s\Pi_0(\Gamma_0 - \Pi_0) + 3\Pi_0\Gamma_0 + \Gamma_0^2 \pm 2\Gamma_0(1 + BC_s)\sqrt{\frac{\Pi_0\Gamma_0}{BC_s}}}{(\Gamma_0 - BC_s\Pi_0)^2} \quad (72)$$

Moreover, $D > 0$ if $\lambda < \lambda_a^-$ or $\lambda > \lambda_a^+$. Since $\Pi_0 < \beta^- < \Gamma_0$, we always have $\lambda_a^+ > 0$ and it may be verified that $\alpha_\Pi(\lambda) < 0$ for all $\lambda \in [\lambda_a^+, 1]$, so that we can limit our attention to λ_a^- . Using $BC_s + 2 - 2\sqrt{1 + BC_s} = \left(1 - \sqrt{1 + BC_s}\right)^2$, we can show that $\lambda_a^- = 0$ if $\Pi_0 = \beta^-$ and $\lambda_a^- > 0$ if $\Pi_0 < \beta^-$. Furthermore, it can be shown that $\alpha_\Pi(0) = x_b$ and $\alpha_\Pi(\lambda) > x_b$ for $0 < \lambda \leq \lambda_a^-$. This makes perfect sense in terms of the solution in region II: at $t = \tau_b$, the boundary curve hits the characteristic corresponding to $\lambda = 0$. The boundary curve then intersects with subsequent neighbouring characteristics until $\lambda = \lambda_a^-$, after which $\alpha_\Pi(\lambda)$ stops being real-valued. Using Eqs. (67)–(72) (and after a lot of algebra), it can actually be proved that $\tilde{C}_2(\alpha_\Pi(\lambda_a^-), \lambda_a^-) = \xi_a = y_a^-$ [from Eq. (55)] and $V_\Pi(\lambda_a^-) = V_L(\xi_a)$. This verifies the invariance of Eq. (33) between solution regions II and III. As before, we now define $x_a := \alpha_\Pi(\lambda_a^-)$, $\tau_a := \tilde{t}_2(0, \lambda_a^-)$. The characteristic $t = \tilde{t}_2(x, \lambda_a^-)$ is tangent to the boundary curve at (x_a, τ_a) . As in Case 2a (Fig. 15), a new region IV will exist for $t \geq \tau_a$ in which the solution is a travelling wave of velocity $U_3 := V_L(\xi_a) = V_\Pi(\lambda_a^-)$. This region is enclosed by the curve $t = \tilde{t}_2(x, \lambda_a^-)$ and the boundary $x = \alpha_\Pi(t) = x_a + U_3(t - \tau_a)$.

During the time interval $[t^*, \tau_a]$, the motion of α_Π determines a nonzero solution in Ω_0 . For $t^* \leq t \leq \tau_b$, this pure adsorption solution is given by Eq. (66). A similar relation applies for $\tau_b \leq t \leq \tau_a$: given an arbitrary concentration value $c \in [\xi_b, \xi_a]$, we solve $c = \tilde{C}_2(\alpha_\Pi(\lambda_c), \lambda_c)$ for λ_c to obtain the time $\tilde{t}_2(\alpha_\Pi(\lambda_c), \lambda_c)$. For $t \geq \tilde{t}_2(\alpha_\Pi(\lambda_c), \lambda_c)$, the velocity of c is $V_L(c)$. This is expressed in the following relation:

$$x = \alpha_\Pi(\lambda_c) + V_L(c) \cdot (t - \tilde{t}_2(\alpha_\Pi(\lambda_c), \lambda_c)) \quad (73)$$

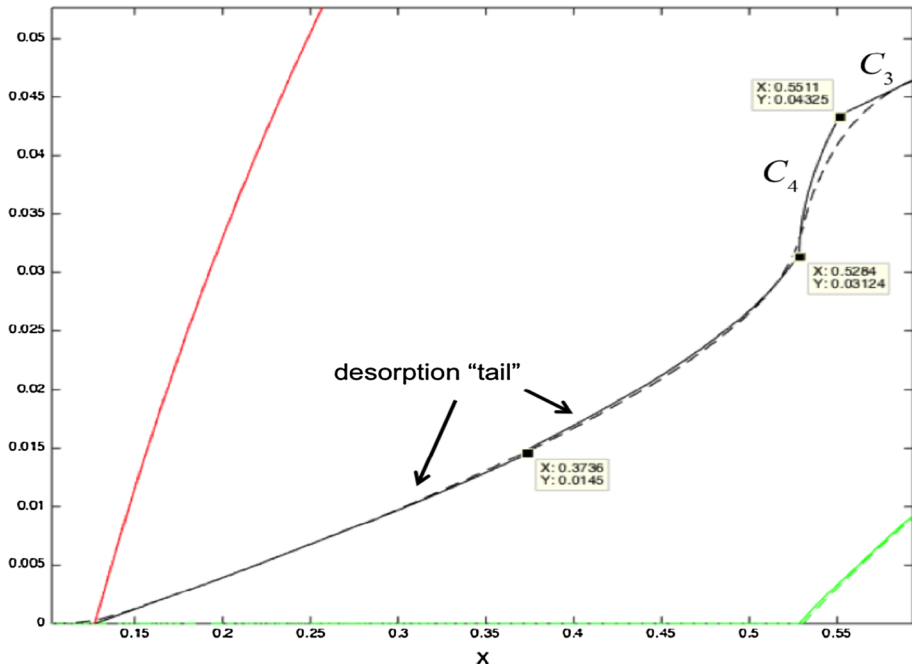


Fig. 22 Close-up of solution profiles of Example 3 at $t = 2 > \tau_d$

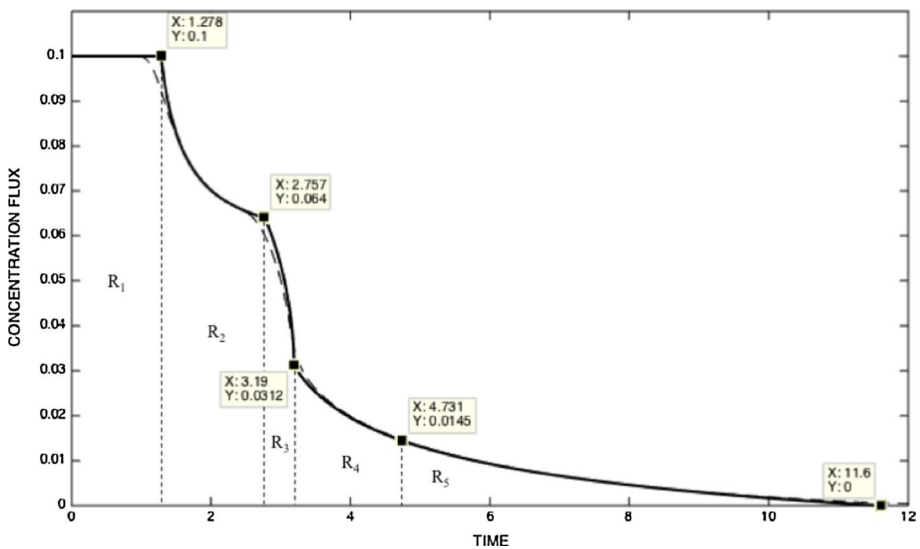


Fig. 23 Effluent concentration flux for Example 3

evolution of the discontinuity in the Cauchy data at $x = 0$, $t = 0$. This solution exhibits a mixture of the shock discontinuity found in the case of “pure precipitation” ($\Gamma_{eq} = 0$) and the rarefaction wave solution for the case of “pure equilibrium adsorption” ($\kappa = 0$).

The introduction of the parameter λ also allowed for the construction of the precipitate profile, $\Pi(x, t)$, and we showed that $\Pi > 0$ on Ω for all $t < t^* = \Pi_0/\kappa C_s$. An expression for the velocity of an arbitrary precipitate value P in terms of the corresponding concentration level C_P was found [see Eq. (33)]. The assumption that this relationship is “invariant” between all solution regions leads to the equation of motion of the point α_Π [Eq. (35)]. If $\alpha'_\Pi(t^*) \leq V_L(0)$ (“Case 1”), we saw that a travelling wave solution emerged immediately and the concentration and precipitate profiles behind it were identical zero. On the other hand, if $\alpha'_\Pi(t^*) > V_L(0)$ (“Case 2”), the solution was characterised by a nonzero pure adsorption tail in the region where the precipitate was used up. This tail continued to form until the velocity of α_Π became equal to the Langmuir velocity of the concentration value at $x = \alpha_\Pi$. It was only at this stage that a travelling wave component began to emerge. The solutions thus constructed were tested for mass conservation by integration of the effluent concentration flux profile and further validated by comparison with numerical solutions in a few example cases.

6.1 Effluent Concentration Profiles

This work has primarily been concerned with the construction of the in situ solution profiles, without paying special attention to the finite length L of the rock core. However, in a laboratory setting, the principal measurable quantity is the effluent concentration $C(L, t)$. The variation of this level with time can tell us which regime (desorption or dissolution) is more prominent. It also determines the “lifetime” of a squeeze treatment, the amount of time that the effluent concentration is at least equal to a threshold level C_t below which scale inhibition becomes ineffective. In order to address these matters in terms of the various parameters, we briefly recall the three qualitatively different in situ profiles found in Sects. 4 and 5. They can be distinguished purely in terms of the (uniform) initial levels of precipitation (Π_0) and adsorption ($\Gamma_0 = \Gamma_{eq}(C_s)$). To this end, we write $\Gamma_{eq}(C) = B\Gamma_{max}C/(1 + BC)$ and introduce the functions

$$P_1(\Gamma_0) := \frac{\Gamma_0^2}{\Gamma_{max} - \Gamma_0} \quad (74)$$

$$P_2(\Gamma_0) := \Gamma_0 + 2(\Gamma_{max} - \Gamma_0) - 2\sqrt{\Gamma_{max}(\Gamma_{max} - \Gamma_0)} \quad (75)$$

Here, Γ_{max} is the maximum amount of scale inhibitor that can be retained on the rock surface through adsorption. If $\Pi_0 \geq P_1(\Gamma_0)$, a travelling wave solution emerges at $t = t^*$ (Case 1). On the other hand, if $\Pi_0 < P_1(\Gamma_0)$, then we have $d\alpha_\Pi/dt > V_L(C(\alpha_\Pi, t))$ until $t = \tau_a$ such that $C(\alpha_\Pi, \tau_a) = \xi_a$, where

$$\xi_a = \frac{1}{B} \left[\frac{\Pi_0 + \Gamma_0 - \Gamma_{max} \sqrt{\frac{\Pi_0}{\Gamma_{max} - \Gamma_0}}}{\Gamma_{max} - \Gamma_0 - \Pi_0} \right] \quad (76)$$

If $P_2(\Gamma_0) < \Pi_0 < P_1(\Gamma_0)$, then the point $(\alpha_\Pi(\tau_a), \tau_a)$ is in region III, so ξ_a at that time lies on the steady-state component (Case 2a). Finally, if $\Pi_0 \leq P_2(\Gamma_0)$, then $(\alpha_\Pi(\tau_a), \tau_a)$ is in region II (Case 2b). Prior to this, region III disappears at $t = \tau_b$ such that $C(\alpha_\Pi, \tau_b) = \xi_b$, where

$$\xi_b = \frac{1}{2B} \left[\frac{\Gamma_0 - \Pi_0 - \sqrt{(\Gamma_0 - \Pi_0)^2 - 4\Pi_0(\Gamma_{\max} - \Gamma_0)}}{\Gamma_{\max} - \Gamma_0} \right] \quad (77)$$

The possible effluent concentration profiles are summarised in Fig. 24. We note that all cases with initial precipitate level $\Pi_0 > P_2(\Gamma_0)$ have a “plateau” of constant concentration $C_s - C_s e^{-\kappa L/\nu}$ as a result of the breakthrough of the steady-state component in the in situ profiles. For $\Pi_0 \leq P_2(\Gamma_0)$, this only occurs if $\alpha_{\Pi}(\tau_b) = \nu\kappa^{-1} \ln(1 - \xi_b/C_s) > L$. It should be emphasised that Π_0 , Γ_0 , Γ_{\max} determine which qualitative case (1, 2a, 2b) occurs. The values ξ_a , ξ_b only have an additional explicit dependence on B . Once these are fixed, variations in κ , ν and L cause the emergence and length of particular solution regions in the effluent profiles. In the next sections, we will identify situations in which a desired threshold concentration C_t is to be maintained for as long as possible, taking into account practical constraints on the variables of the system.

6.2 Slow Versus Fast Dissolution

The rate equations in the full scale inhibitor deposition/retention model are governed by the adsorption/desorption rate parameter r_a and the precipitation/dissolution rate parameter κ . There are four limiting behaviours (see Fig. 25), ranging from the fully kinetic case, when both rate parameters are finite, to the full equilibrium case, when both rate parameters are infinite. In practical applications, the rate parameters need to be considered in relation to the length of the system (reservoir or rock core) and the flow rate, which both determine the impact of the two mechanisms on the mobile phase concentration. For instance, in case of a core-flood experiment on rock core of length L , a low flow rate Q implies a

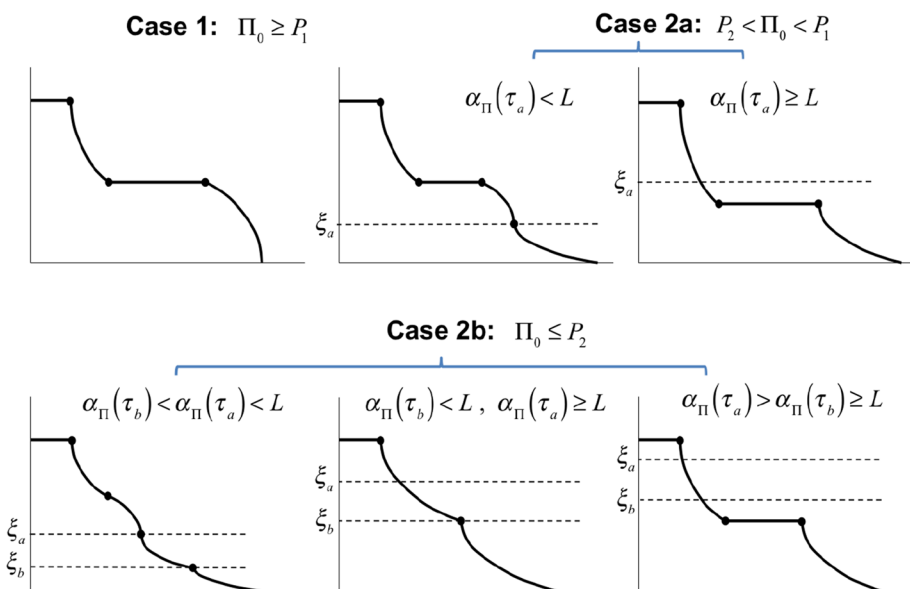


Fig. 24 Possible effluent concentration profiles

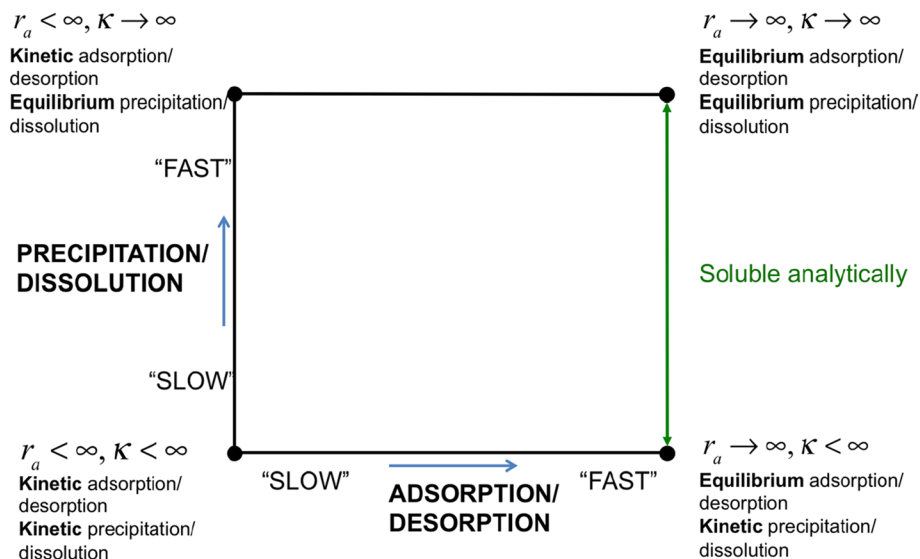


Fig. 25 “Phase diagram” illustrating the different combinations of the adsorption and precipitation mechanisms

low fluid velocity $v = Q/A\phi$ (A = cross-sectional area, ϕ = porosity), which corresponds to a *long* fluid residence time L/v . A high but finite rate parameter can then lead to behaviour that is very similar to an equilibrium process. This is no longer the case if the flow rate is increased significantly. Thus, the rate parameters must be considered relative to the residence time of the fluid, and kinetic/equilibrium-type behaviour can always be achieved by increasing/decreasing v sufficiently. For *fixed* L/v , we say that a desorption/dissolution process is “fast” if it is very close to equilibrium behaviour (typically very high values of κ , r_a). On the other hand, the process is called “slow” if it deviates noticeably from equilibrium (low or medium values of κ , r_a). The analytical solutions found in this paper are for fast adsorption/desorption processes only (i.e. equilibrium adsorption), but capture both slow and fast precipitation/dissolution. Figure 26 illustrates slow versus equilibrium (fast) dissolution in Case 2a. Both in situ profiles are sketched at a time $\tau_a + \Delta t$, when the travelling wave component (IV) is present. Now, as κ is increased, τ_a becomes closer to t^* , which itself decreases due to faster dissolution of the precipitate. Regions II and III become narrower, while IV widens. At the same time, the concentration in these regions gets closer to C_s . In the limit $\kappa \rightarrow \infty$, we have $\tau_a = t^* = 0$ and regions II and III disappear completely. The characteristic separating regions III and IV (see Fig. 15) then collapse onto the characteristic $x = V_L(C_s)t$, and the travelling wave develops a discontinuity at $x = V_L(\xi_a)t$. In order to emphasise the importance of the time τ_a for the effectiveness of a squeeze treatment, we compare the effluent concentration profiles for “slow” versus “fast” dissolution. In the sketch in Fig. 27, it is assumed that the threshold concentration is $C_t < \xi_a$ and that $\alpha_H(\tau_a) = \nu\kappa^{-1} \ln(1 - \xi_a/C_s) < L$, so that the travelling wave can be seen in the effluent profile. We observe that fast (equilibrium) dissolution sustains the concentration level $C = C_s$ before dropping off sharply to ξ_a and decreasing further down to the threshold concentration. The lifetime of the squeeze treatment now depends solely on the Langmuir speed $V_L(C_t)$, as indicated by the red dashed line. If scale inhibitor is just as effective at threshold concentration as it is for higher concentrations, then the fast dissolution process

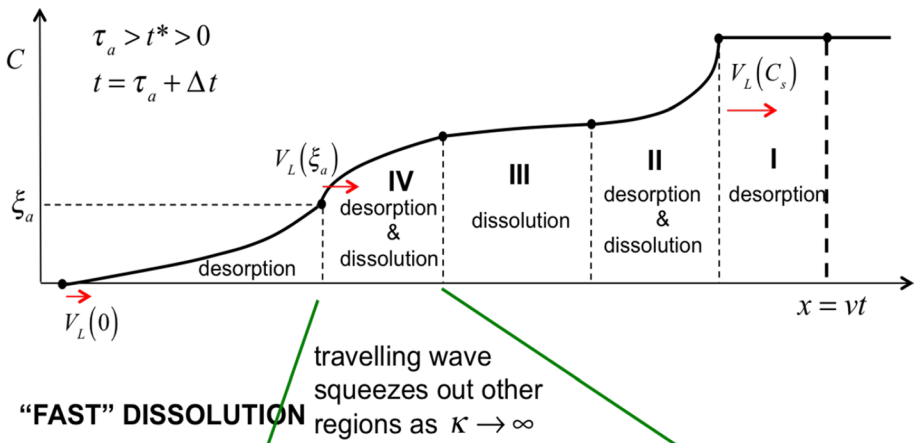
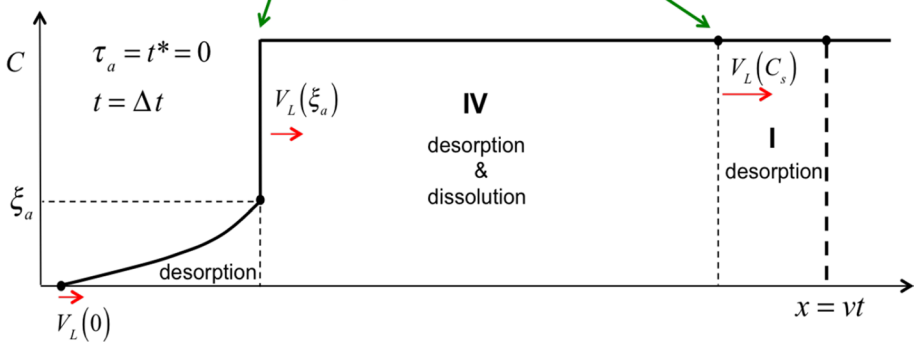
“SLOW” DISSOLUTION**“FAST” DISSOLUTION**

Fig. 26 In situ profiles for $\kappa < \infty$ (top) and $\kappa \rightarrow \infty$ (bottom)

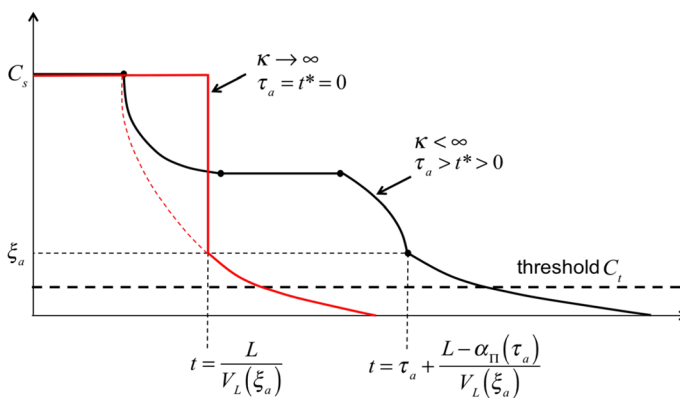


Fig. 27 Effluent profiles for $\kappa < \infty$ and $\kappa \rightarrow \infty$

is not economic at all in this case, because a pure adsorption/desorption squeeze treatment would achieve exactly the same lifetime. The initial mobile phase concentration for such a treatment just needs to be equal to C_t , far below the solubility level C_s . This evidently requires much less scale inhibitor than the coupled process, in which the injected concentration needs to be greater than C_s in order for the precipitate to form (virtually always the case in practice). All this extra scale inhibitor is “wasted” if it just results in a higher return curve rather than delaying the breakthrough time of C_t . The latter is achieved by the slow (kinetic) dissolution mechanism, mainly because of the resulting increase in t^* . In order to optimise usage of the available precipitate, the plateau of concentration $C_s - C_s e^{-\kappa L/v}$ should be as close to the threshold level C_t as possible (just above, in fact). For a given rate parameter κ , such a low return curve can be obtained by increasing the flow rate. In terms of produced pore volumes, this results in the same lifetime while ensuring optimal usage of the scale inhibitor in the system. Moreover, we should bear in mind that the model with constant fluid velocity only applies to core-flooding experiments. In case of a producing well in the field, the fluid velocity is inversely proportional to the radial distance from the well. In order to predict the return curves accurately, we would of course need to derive an analytical solution for this radial model. However, qualitative predictions can already be made using the solution of the present linear model. Broadly speaking, the same type of solution components will appear in the radial setting, but they will be stretched considerably in the region close to the producing well, where the fluid velocity is very high. Also, if the same parameters are used as input for both models, the effect of dissolution in the radial case will be *less* than in the linear case, due to the shorter fluid residence time. In order to achieve similar concentration levels in both return curves, the flow rate in the radial case will then need to be lowered. This is even more true if precipitate is formed only at a certain distance from the producing, due to low temperatures in the near-well region and higher temperatures further into the reservoir.

6.3 Lifetime Increase Due to Precipitation

We noted above that if the steady-state component appears in the effluent profile, the available precipitate is used in the most efficient way when the flow rate is adjusted to make $C_s - C_s e^{-\kappa L/v} = C_t$. If no adsorption were to occur, this yields a squeeze lifetime (in pore volumes) of exactly

$$T_{\text{pptn}} = \frac{v}{L} \left(1 + \frac{\Pi_0}{\kappa C_s} \right) \quad (78)$$

This lifetime is increased if adsorption is then considered. For example, in Case 1 ($\Pi_0 \geq P_1(\Gamma_0)$), the lifetime of the adsorption/precipitation squeeze treatment is found by calculating when the characteristic separating the steady-state and travelling wave components intersects with the line $x = L$. The characteristic is given by equation (42), from which it follows that

$$T_{\text{ads/pptn}} = T_{\text{pptn}} + \frac{v}{\kappa L} \left[\kappa \Gamma'_0 + \Gamma'_0 \ln(1 + BC_t) + \frac{\Gamma_0}{C_s} \frac{BC_t}{1 + BC_t} \right] \quad (79)$$

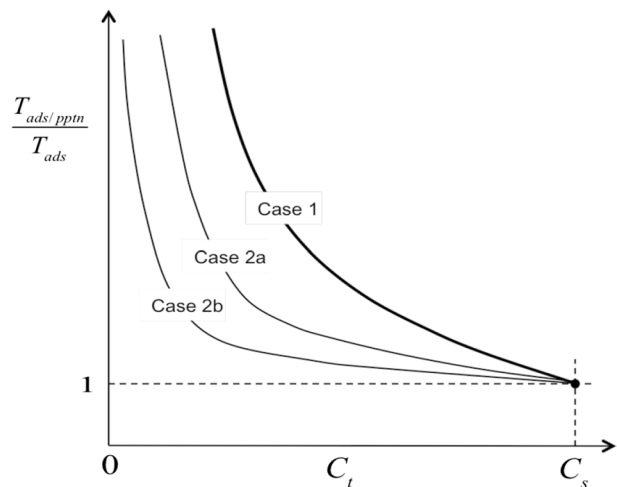
where $\Gamma_0 = \Gamma_{\text{eq}}(C_s)$, $\Gamma'_0 = \Gamma'_{\text{eq}}(C_s)$ and $C_t = C_s - C_s e^{-\kappa L/v}$. The last term shows the addition in lifetime due to adsorption. The percentage increase with respect to T_{pptn} is actually limited due to the inter-dependence of the parameters involved. For instance, an increase in

the adsorption capacity Γ_{\max} will cause both Γ_0 and Γ'_0 to increase. However, for larger increases, we will have to increase Π_0 accordingly in order to stay in Case 1. This evidently caps the proportional increase in lifetime, since it increases T_{pptn} . Similarly, changes in B or C_s might increase Γ_0 , but simultaneously decrease Γ'_0 . Although only a rigorous analysis will reveal what combinations of parameters maximise the “extra lifetime term” in Eq. (79), we can make some general observations regarding this issue. Notice that, on the one hand, the lifetime tends to $v/L(1 + \Gamma'_0)$ pore volumes as $\kappa \rightarrow \infty$ ($C_t \rightarrow C_s$), corresponding to the retardation of the value C_s due to desorption. On the other hand, it can be shown that, as $\kappa \rightarrow 0$, the last term in Eq. (79) becomes $v/\Gamma'_0 L + BC_s \Gamma'_0 + B\Gamma_0$. Thus, for small κ , we have $T_{\text{ads/pptn}} \approx T_{\text{pptn}} \approx \Pi_0/\kappa C_s$. In order to appreciate the benefits of inducing precipitation, we have to compare $T_{\text{ads/pptn}}$ with $T_{\text{ads}} = v/L(1 + \Gamma'_{\text{eq}}(C_t))$, the lifetime achieved by a pure adsorption treatment. Figure 28 illustrates the variation of the ratio of $T_{\text{ads/pptn}}$ and T_{ads} with the threshold concentration C_t . Large increases in lifetime are observed particularly if the threshold concentration is much lower than the solubility. A similar benefit-analysis can be carried out in Cases 2a and 2b (also sketched in Fig. 28). Here, the advantage of inducing precipitation is less prominent for higher threshold values. This is already obvious from the effluent profiles in Fig. 24. In Case 2b for instance, the effects of desorption can outweigh dissolution so much that the steady-state component is never able to break through. This is because either the amount of precipitate is very low or the isotherm is initially very steep and then levels off, causing Γ_0 to be close to Γ_{\max} . Compared to pure adsorption, the squeeze lifetime is still improved, but less so than in Case 1 or 2a. Eventually, when κ is decreased or v is increased (and hence C_t lowered) to such an extent that $\alpha_{\text{II}}(\tau_b) < L$, the steady-state will appear in the effluent profile, resulting in larger percentage improvements.

6.4 Lifetime Dependence on Desorption

In the previous sections, we considered how dissolution improves squeeze lifetime. In that discussion, it was assumed that the flow rate can always be adjusted to make $C_t = C_s - C_s e^{-\kappa L/v}$, so that the lifetime is defined by the length of the steady-state plateau

Fig. 28 Illustration of the beneficial effect of inducing precipitation



in the effluent concentration profiles (except possibly in Case 2b). However, in practice, it might not be possible to increase the flow rate to this extent. We could have a situation in which, at the fastest possible flow rate, the effluent concentration level $C_s - C_s e^{-\kappa L/v}$ is still much higher than C_t (as was shown in Fig. 27). The lifetime then depends significantly on the nature of the desorption mechanism, which is governed by the Langmuir isotherm. A steep rising isotherm with a high adsorption capacity Γ_{\max} will cause the lower concentration values in the pure desorption tail (present in Cases 2a and 2b) to propagate slowly. Dissolution improves this further, by delaying the advance of C_t . However, as we saw previously, for very steep isotherms, the improvement on the lifetime achieved by a pure adsorption treatment is limited. In such circumstances, inducing precipitation is only worthwhile if a lot of scale inhibitors can be injected. This will increase Π_0 , making the improvement due to dissolution more significant. We then benefit from the “delay” caused by dissolution as well as the slow Langmuir velocity of C_t .

There is another aspect involved with flow rate changes. In the discussion, thus far the adsorption/desorption process was always fast (at equilibrium), whereas precipitation/dissolution could be fast or slow (kinetic). This applies if the desorption rate parameter r_a is very high in relation to the fluid residence time L/v . Thus, large increases in the flow rate could lead to adsorption/desorption becoming kinetic too, so that the bottom left corner of the “phase diagram” in Fig. 25 applies. In this case, the system can only be solved numerically, which we have done but space considerations prevent the inclusion of these results here. However, our findings highlighted the importance of the ratio κ/r_a . For instance, if precipitation is slow with $\kappa = 10$ and adsorption is fast with $r_a = 100$, then making the flow rate ten times faster effectively decreases the rate parameters to $\kappa = 1$ and $r_a = 10$. Both processes are now slow in the sense that the solution profiles clearly show some deviation compared to the $r_a \rightarrow \infty$ case, and we found that the effect on squeeze lifetime will be rather limited. This may change for high values of κ/r_a , when desorption is slow compared to dissolution. Then, if the threshold concentration is sufficiently low, the squeeze lifetime may be increased hugely due to very long pure adsorption tails.

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References

- Akanji, L., Falade, G.: Closed-form solution of radial transport of tracers in porous media influenced by linear drift. *Energies* **12**(1), 29 (2019)
- Alinhac, S.: *Hyperbolic Partial Differential Equations*. Springer, Berlin (2009)
- Amjad, Z., Demadis, K.: *Mineral Scales and Deposits: Scientific and Technological Approaches*. Elsevier, Amsterdam (2015)
- Holden, H., Risebro, N.: *Front Tracking for Hyperbolic Conservation Laws*. Springer, Berlin (2002)
- Kahrwad, M., Sorbie, K.S., Boak, L.S.: Coupled adsorption/precipitation of scale inhibitors: experimental results and modeling. *Soc. Pet. Eng.* **24**, 481–491 (2009)

- Kerver, J.K., Heilhecker, J.K.: Scale inhibition by the squeeze technique. *Pet. Soc. Canada* **8**, 15–23 (1969)
- Khormalia, A., Petrakov, D.G., Moghaddam, R.N.: Study of adsorption/desorption properties of a new scale inhibitor package to prevent calcium carbonate formation during water injection in oil reservoirs. *J. Pet. Sci. Eng.* **153**, 257–267 (2017)
- King, G.E., Warden, S.L.: Introductory work in scale inhibitor squeeze performance: core tests and field results. In: *Society of Petroleum Engineers* (1989)
- Lax, P.: Hyperbolic systems of conservation laws II. *Commun. Pure Appl. Math.* **10**, 537–566 (1957)
- Malandrino, A., Yuan, M.D., Sorbie, K.S., Jordan, M.M.: Mechanistic study and modelling of precipitation scale inhibitor squeeze processes. In: *Society of Petroleum Engineers* (1995)
- Meyers, K.O., Skillman, H.L., Herring, G.D.: Control of formation damage at Prudhoe Bay, Alaska, by inhibitor squeeze treatment. *Soc. Pet. Eng.* **37**, 1019–1034 (1985)
- Miles, L.: A new concept in scale inhibitor formation squeeze treatments. In: *Society of Petroleum Engineers* (1970)
- Ockendon, J., Howison, S., Lacey, A., Movchan, A.: *Applied Partial Differential Equations*. Oxford University Press, Oxford (2003)
- Ramirez, W., Shuler, P., Friedman, F.: Convection, dispersion, and adsorption of surfactants in porous media. *Soc. Pet. Eng.* **20**, 430–438 (1980)
- Safari, H., Jamialahmadi, M.: Thermodynamics, kinetics, and hydrodynamics of mixed salt precipitation in porous media: model development and parameter estimation. *Transp. Porous Media* **101**(3), 477–505 (2014)
- Smoller, J.: *Shock-Waves and Reaction–Diffusion Equations*. Springer, Berlin (1994)
- Sorbie, K.S.: A general coupled kinetic adsorption/precipitation transport model for scale inhibitor retention in porous media: I. Model formulation. In: *Society of Petroleum Engineers* (2010)
- Sorbie, K.S.: A simple model of precipitation squeeze treatments. In: *Society of Petroleum Engineers* (2012)
- Sorbie, K.S., Stamatiou, A.: Analytical solutions of a one-dimensional linear model describing scale inhibitor precipitation treatments. *Transp. Porous Media* **123**, 271–287 (2018)
- Sorbie, K., Yuan, M., Todd, A., Wat, R.: The modelling and design of scale inhibitor squeeze treatments in complex reservoirs. In: *Society of Petroleum Engineers* (1991)
- Sorbie, K.S., Wat, R.M.S., Todd, A.C.: Interpretation and theoretical modeling of scale-inhibitor/tracer corefloods. *Soc. Pet. Eng.* **7**, 307–312 (1992)
- Stiff, H., Davis, L.: A method for predicting the tendency of oil field waters to deposit calcium sulfate. *J. Pet. Technol.* **195**, 25–28 (1952)
- Trogus, F., Sophany, T., Schechter, R.S., Wade, W.: Static and dynamic adsorption of anionic and nonionic surfactants. *Soc. Pet. Eng.* **17**, 337–344 (1977)
- Vazquez, O., Sorbie, K.S., Mackay, E.J.: A general coupled kinetic adsorption/precipitation transport model for scale inhibitor retention in porous media: II. Sensitivity calculations and field predictions. In: *Society of Petroleum Engineers* (2010)
- Vetter, O.J.: The chemical squeeze process some new information on some old misconceptions. *Soc. Pet. Eng.* **25**, 339–35 (1973)
- Yuan, M.D., Sorbie, K.S., Todd, A.C., Atkinson, L.M., Riley, H., Gurden, S.: The modelling of adsorption and precipitation scale inhibitor squeeze treatments in north sea fields. In: *Society of Petroleum Engineers* (1993)
- Zhang, H., Mackay, E.J., Chen, P., Sorbie, K.S.: Non-equilibrium adsorption and precipitation of scale inhibitors: corefloods and mathematical modelling. In: *Society of Petroleum Engineers* (2000)